### Appendix A to FAR 99-06

# ENERGY INNOVATIONS SMALL GRANT (EISG) PROGRAM

### **EISG FINAL REPORT**

## RENEWABLE HYDROGEN FUEL PRODUCTION BY MICROALGAL PHOTOSYNTHESIS

### **EISG AWARDEE**

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### **Executive Summary**

### 1. Introduction

Recent work has shown that lack of sulfur from the growth medium of green algae caused a hitherto unknown switch in cellular photosynthesis. In sealed cultures, instead of oxygen gas, green algae produced hydrogen gas (Melis et al., 2000). It was shown that, under such sulfur-deprivation conditions, it is possible to photoproduce and to accumulate significant volumes of  $H_2$  gas, using the green alga *Chlamydomonas reinhardtii*, in a sustainable process that can be employed continuously for several days. Thus, progress was achieved by a temporal separation of the reactions of (I) normal photosynthesis, cell growth, carbohydrate accumulation and  $O_2$  production from (II) anaerobic photosynthesis and  $H_2$  production. This process became known as the "Two-Stage Photosynthesis and  $H_2$ -Production" process (Melis et al., 2000). The novel application of this two-stage protocol revealed the occurrence of hitherto unknown metabolic, regulatory and electron-transport pathways in the green alga *C. reinhardtii* (Melis et al., 2000; Zhang et al. 2001), leading to the significant and sustainable light-dependent release of  $H_2$ -gas by the cells.

The temporal sequence of events in this two-stage photosynthesis and  $H_2$ -production process is as follows.

- Green algae are grown photosynthetically in the light (normal photosynthesis) until they reach a density of 3-6 million cells per ml in the culture.
- Sulfur deprivation is imposed upon the cells in the growth medium, either by carefully limiting sulfur supply in the medium so that it is consumed entirely, or by permitting cells to concentrate in the growth chamber prior to replacement of the growth medium with one that lacks sulfur nutrients. Cells respond to this S-deprivation by fundamentally altering photosynthesis and cellular metabolism in order to survive (Davies et al., 1996; Hell, 1997; Zhang et al., 2001).
- Inorganic S-deprivation in *C. reinhardtii* exerts a distinctly different effect on the cellular activities of photosynthesis and respiration. The activity of photosynthesis, measured from the light-saturated rate of O<sub>2</sub> evolution, declines quasi-exponentially with a half-time of 15-20 h to a value less than 10% of its original rate (Wykoff et al., 1998). However, cellular respiration, measured from the rate of O<sub>2</sub> consumption in the dark, remains fairly constant over the S-deprivation period (Melis et al., 2000). In consequence, the absolute activity of photosynthesis slips to a level below that of respiration after about 24 h of S-deprivation. Following this crosspoint, sealed cultures of S-deprived *C. reinhardtii* quickly consume all dissolved oxygen and become anaerobic (Ghirardi et al., 2000), even though they are maintained under continuous illumination.
- Under S-deprivation conditions, sealed (anaerobic) cultures of *C. reinhardtii* produce H<sub>2</sub> gas in the light but not in the dark. The volume and rate of photosynthetic H<sub>2</sub> production was monitored from the accumulating H<sub>2</sub> gas in an inverted graduated burette, measured from the

volume of water displacement. A rate of 2.0-2.5 mL H<sub>2</sub> production per liter culture per hour was sustained in the 24-70 h period. The rate declined gradually thereafter.

### 2. Project Objectives

A project objective was to improve in the laboratory the novel Two-Stage Photosynthesis and H<sub>2</sub>-Production process and to develop/employ conditions for the continuous production of hydrogen gas. A further objective was to obtain better insight into the biochemistry of the process and the physiology of the cells as they produce H<sub>2</sub> gas under sulfur deprivation. This knowledge is pivotal in efforts to increase the yield and commercialize the process.

### 3. Project Outcomes

A summary of what we have learned from the conduct of this work is given below:

- In the presence of S, green algae do normal photosynthesis (H<sub>2</sub>O oxidation, O<sub>2</sub> evolution and biomass accumulation). The absence of sulfur from the growth medium of green algae acts as a metabolic switch, one that <u>selectively</u> and <u>reversibly</u> turns-off photosynthetic O<sub>2</sub> production.
- In the absence of S and absence of O<sub>2</sub>, photosynthesis in *C. reinhardtii* slips into the H<sub>2</sub> production mode.
- Reversible application of the switch (presence/absence of S) permits the algae to alternate between O<sub>2</sub> production/biomass accumulation and H<sub>2</sub> production (temporal separation of the two processes), thus bypassing the incompatibility and mutually exclusive nature of the O<sub>2</sub> and H<sub>2</sub> producing reactions.
- Interplay between oxygenic photosynthesis, mitochondrial respiration, catabolism of endogenous substrate, and electron transport via the hydrogenase pathway is essential for this light-mediated H<sub>2</sub>-production process.
- The release of H<sub>2</sub> gas serves is an alternative (and novel) light-mediated "respiration" by the cells, needed for the survival of the organism under sulfur-deprivation conditions.

### 4. Conclusions

Upon further refinement, the "Two-Stage Photosynthesis and H<sub>2</sub>-Production" process may serve in the generation of H<sub>2</sub> gas for the fuel and chemical industries. There are no absolute technical barrier for the application of this technology in the commercial production of H<sub>2</sub> gas.

### 5. Benefits to California

Both small-scale (industrial and commercial) and larger (utility) solar energy conversion plants (photobioreactors) can be envisioned utilizing the Two-Stage Photosynthesis and  $H_2$ -

Production process. Remote photobioreactors could be installed as modules in arid areas where sunlight is plentiful and alternative uses of land are minimal. Such a process of  $H_2$  gas production would be sustainable, environmentally friendly and economically attractive compared to most other alternatives.

In addition to  $H_2$ , a valuable and clean fuel, the Two-Stage Photosynthesis and  $H_2$ -Production process will generate green algal biomass as a significant "Value-Added Bioproduct" that will enhance the economics and competitiveness of the process. In sum, the process will find application in the:

- Generation of a valuable, clean and renewable fuel.
- Global warming mitigation and reduction in the level of atmospheric polution.
- Production of biomass from which "High-value Bioproducts and Biochemicals" could be extracted.

### 6. Recommendations

The "Two-Stage Photosynthesis and  $H_2$ -Production" process brings together two normally separate fields: Energy and Biotechnology. The successful development and employment of this method will boost California's competitiveness in the fields of Energy, Agriculture and Chemistry.

It is thus recommended that every effort be made to advance this technology to its fullest potential

### **Abstract**

Sulfur-deprivation in green algae causes reversible inhibition in the activity of photosynthesis. In the absence of sulfur, rates of photosynthetic O2 evolution drop below those of O<sub>2</sub> consumption by respiration. In consequence, sealed cultures of the green alga Chlamydomonas reinhardtii become anaerobic in the light, induce the "Fe-hydrogenase" pathway of electron transport and photosynthetically produce H<sub>2</sub> gas. In the course of such H<sub>2</sub> gas production, cells consume significant amounts of internal starch and protein. Such catabolic reactions may sustain, directly or indirectly, the H<sub>2</sub>-production process. Reversible application of the switch (presence/absence of S) permits the algae to alternate between O production/biomass accumulation and H<sub>2</sub> production (temporal separation of the two processes), thus bypassing the incompatibility and mutually exclusive nature of the O2 and H2 producing reactions. Repetitive application of the switch could be the basis of a commercial H<sub>2</sub>-production system. Profile analysis of selected photosynthetic proteins during H<sub>2</sub>-production showed a precipitous decline in the amount of Rubisco as a function of time in S-deprivation. It is suggested that, under Sdeprivation conditions, electrons derived from a residual photosynthetic H<sub>2</sub>O-oxidation activity and from endogenous substrate catabolism feed into the hydrogenase pathway, thereby contributing to the H<sub>2</sub>-production process in *Chlamydomonas reinhardtii*. Interplay between oxygenic photosynthesis, mitochondrial respiration, catabolism of endogenous substrate, and electron transport via the hydrogenase pathway is essential for this light-mediated H<sub>2</sub>-production process. The promise and application of this technology in the fields of Energy, Agriculture and Chemistry are discussed.

**Keywords** *Chlamydomonas reinhardtii* – Green algae – Hydrogen production – Hydrogenase – Photosynthesis – Sulfur deprivation

### **Main Report**

### Introduction

### Background and Overview

Hydrogen gas is considered as the ideal fuel for a California future in which air pollution has been eliminated, global warming has been arrested and our environment has been protected in an economically sustainable manner. Hydrogen fuel would team with electricity to provide attractive options to Californians in transportation and power generation. The easiness of interconversion between these two forms of energy suggests a future in which the electric power grid would become a carrier, user and producer of hydrogen, depending on local conditions and many interdependent and only partially predictable technological developments. Achieving this vision as a practical reality within the next century will require a significant effort in order to attain the necessary infrastructure in H<sub>2</sub> production and utilization technologies. The most challenging problem in establishing hydrogen as a fuel for the future is the renewable generation of large quantities of hydrogen gas. Thus, processes that are presently conceptual in nature, or at an early development stage in the laboratory, need to be encouraged, tested for feasibility and assessed to identify the most promising alternatives.

Since the pioneering discovery by Gaffron and co-workers over 60 years ago (Gaffron 1939; Gaffron and Rubin, 1942), the ability of unicellular green algae to produce  $H_2$  gas in the light has been mostly a biological curiosity. Historically, hydrogen evolution activity in green algae was elicited upon a period of <u>anaerobic incubation of the cells in the dark</u> (Greenbaum, 1982; Roessler and Lien, 1984; Happe and Naber, 1993). A high specific activity hydrogenase enzyme was expressed under such incubation of the cells and catalyzed a light-mediated  $H_2$ -evolution. The monomeric form of the enzyme, which belongs to a novel class of Fehydrogenases (Voordouw et al., 1989; Adams, 1990; Meyer and Gagnon, 1991; Peters et al., 1998) is encoded in the nucleus of the unicellular green algae but the mature protein is localized and functions in the chloroplast stroma (Happe et al., 1994). Light absorption by the photosynthetic apparatus is essential for the generation of hydrogen. Ferredoxin PetF, the natural electron donor, links the Fe-hydrogenase to the photosynthetic electron transport chain of the green algae (Florin et al., 2001). However, light absorption also results in the oxidation of  $H_2O$  and the release of molecular  $O_2$ , which is a powerful inhibitor of the Fe-hydrogenase.

In addition to this PSII-dependent  $H_2$  photoevolution, which implicates water as the source of electrons and produces 2:1 stoichiometric amounts of  $H_2$  and  $O_2$ , a second mechanism has been described in the literature (Gfeller and Gibbs, 1984). The alternative pathway entails catabolism of endogenous substrate and an oxidative carbon pathway for the generation of reducing power in the chloroplast of the green algae. Reductant (electrons) from such endogenous substrate catabolism feeds into the photosynthetic electron-transport chain between the two photosystems, and probably at the level of the plastoquinone pool. Light absorption by PSI and the ensuing electron transport elevates the redox potential of these electrons to the redox equivalent of ferredoxin (Gibbs et al., 1986). Thus, following a sufficiently dark anaerobic incubation of the culture, high amounts of  $H_2$  can be transiently detected upon a subsequent illumination of the algae (Happe and Naber, 1993; Ghirardi et al., 1997).

The transient only nature of  $H_2$ -production is attributed to the light-dependent simultaneous generation of  $O_2$  by the photosynthetic apparatus. Oxygen is a powerful inhibitor of the Fe-hydrogenase (Ghirardi et al., 2000). Current technological developments in this field

have not yet succeeded in overcoming this mutually exclusive nature of the  $O_2$  and  $H_2$  photoproduction reactions. Thus, the physiological significance and role of the Fe-hydrogenase in green algae, which normally grow under aerobic photosynthetic conditions, has long been a mystery. Given the  $O_2$  sensitivity of the Fe-hydrogenase and the prevailing oxidative environmental conditions on earth, questions have been asked as to whether the hydrogenase is anything more than a relic of the evolutionary past of the chloroplast in green algae, and whether this enzyme and the process of photosynthesis can ever be utilized to generate  $H_2$  gas for commercial purposes (Zhang et al., 2001). Nevertheless, the ability of green algae to photosynthetically generate  $H_2$  gas has captivated the fascination and interest of the scientific community because of the fundamental and practical importance of the process. Below is an itemized list of the properties and promise of photosynthesis in green algal  $H_2$ -production, and the problems that are encountered with current technology:

- Photosynthesis can operate with a photon conversion efficiency of ≥80% (Ley and Mauzerall 1982).
- Microalgae can produce H₂ photosynthetically with a photon conversion efficiency of ≥80% (Greenbaum 1988).
- Molecular O<sub>2</sub> acts as a <u>powerful</u> and <u>effective</u> switch by which the H<sub>2</sub>-production activity is turned off.
- This incompatibility in the simultaneous O<sub>2</sub> and H<sub>2</sub> photoproduction could not be overcome in 60 years of related research.

Recent work has shown that lack of sulfur from the growth medium of the green alga *Chlamydomonas reinhardtii* causes a specific but reversible decline in the rate of oxygenic photosynthesis (Wykoff et al. 1998) but does not affect the rate of mitochondrial respiration (Melis et al., 2000). In sealed cultures, such imbalance in photosynthesis-respiration resulted in a net consumption of oxygen, quickly causing anaerobiosis in the growth medium, a condition that automatically elicited H<sub>2</sub>-production by the cells (Melis et al., 2000). It was shown that, under such conditions, it is possible to photoproduce and to accumulate significant volumes of H<sub>2</sub> gas, using the green alga *Chlamydomonas reinhardtii*, in a sustainable process that can be employed continuously for several days. Thus, progress was achieved by circumventing the sensitivity of the Fe-hydrogenase to O<sub>2</sub> through a temporal separation of the reactions of O<sub>2</sub> and H<sub>2</sub> production, via a so-called "Two-Stage Photosynthesis and H<sub>2</sub>-Production" process (Melis et al., 2000). The novel application of this two-stage protocol revealed the occurrence of hitherto unknown metabolic, regulatory and electron-transport pathways in the green alga *C. reinhardtii* (Melis et al., 2000; Zhang et al. 2001), leading to the significant and sustainable light-dependent release of H<sub>2</sub>-gas by the cells.

Upon further refinement, this method may serve in the elucidation of the green alga hydrogen-related metabolism and in the generation of  $H_2$  gas for the fuel and chemical industries. A summary of the advancement in the state-of-the-art in this field is given below:

- The absence of sulfur from the growth medium triggers a metabolic switch, one that <u>selectively</u> and reversibly turns-off photosynthetic O<sub>2</sub> production.
- In the presence of S, green algae do normal photosynthesis (H<sub>2</sub>O oxidation, O<sub>2</sub> evolution and biomass accumulation). In the absence of S and absence of O<sub>2</sub>, photosynthesis in *C*. *reinhardtii* slips into the H<sub>2</sub> production mode.

### Project Objectives

The discovery of sustainable H<sub>2</sub> production that bypasses the sensitivity of the reversible hydrogenase to O<sub>2</sub> is a significant development in the field. It may lead to exploitation of green algae for the production of H<sub>2</sub> gas as a clean and renewable fuel. However, the actual rate of H<sub>2</sub> gas accumulation was at best 15-20% of the photosynthetic capacity of the cells, when the latter is based on the capacity for O<sub>2</sub> evolution (Melis et al., 2000). The relatively slow rate of H<sub>2</sub>production suggests that there is room for significant improvement in the yield of the process, by as much as one order of magnitude. Similarly, other improvements must be made to optimize the process under conditions of mass culture of the algae. For example, optical problems associated with the size of the chlorophyll antenna and the light-saturation curve of photosynthesis must also be addressed (Melis et al., 1999) before green algae can achieve high photosynthetic solar conversion efficiencies in mass culture. Moreover, H<sub>2</sub>-production by S-deprived algae cannot be sustained forever. The yield begins to level off after about 70 h in S-deprivation. The cells need to go back to normal photosynthesis after about 100 h of S-deprivation in order to be rejuvenated by replenishing lost endogenous substrate (Ghirardi et al. 2000). Thus, it was the objective of this research to perform experimentation by which (a) to improve the yield of the process and (b) to address the continuity of H-production. The work was divided into four specific tasks and was implemented in its entirety. A listing of the tasks is given below:

- <u>Task 1</u>. Improve the  $H_2$  production by shifting forward the equilibrium of the *reversible hydrogenase* catalyzed reaction.
- $\underline{\text{Task 2}}$ . Design and test cell growth media that accentuate the metabolism of  $H_2$  production.
- Task 3. Test the effect of diurnal cycles on starch mobilization and H<sub>2</sub> production.
- Task 4. Identify the rate-limiting step in the H<sub>2</sub> production process.

### **Project Approach and Outcomes**

Task 1: To improve the yield of  $H_2$  production by shifting forward the chemical equilibrium of the reversible hydrogenase catalyzed reaction

Subtask 1: Degassing of the photobioreactor was tested for its effect on the Stage  $1 \rightarrow Stage 2$   $H_2$ —production process.

Experimentation addressed the effect of oxygen partial pressure on the onset of the hydrogen production process. **Figure 1** shows the results of an experiment in which the green algal samples were grown in the photobioreactor until they reached a density of  $3x10^6$  cells per milliliter of culture. Sulfur was removed from the growth medium at time 0 h and the culture was incubated for 24 hours to permit cells to consume internally stored sulfur. The photobioreactor was either degassed for 10 min by a steady stream of argon to purge dissolved atmospheric air from the medium **(Fig. 1, Degassed)**, or sealed without any prior degassing **(Fig. 1, Control)**. Subsequently, culture bottles (Roux type) were sealed with silicone stoppers tightly fitted with a syringe. Capillary Teflon tubing was attached to the syringe for the collection of gasses. The Teflon tubing was used to conduct  $H_2$  gas (evolved by the algae in the photobioreactor) to an upside-down burette filled with water. The upside-down water-filled

burette was immersed in a beaker also filled with water. Hydrogen gas produced by the culture eventually accumulated in the inverted burette by displacing a equal volume of water. It was measured directly from the graduated divisions of the burette.

It is evident from the results of Figure 1 that degassing of the culture accelerates the onset of H<sub>2</sub> production by the cells. This can be attributed to the removal of dissolved oxygen from the growth medium (lowering of the oxygen partial pressure in the photobioreactor). Independent measurements with an oxygen electrode have shown that such degassing is sufficient to lower the oxygen partial pressure from near saturation levels (270 mmoles O<sub>2</sub> per liter medium) to less than 5 mmoles O<sub>2</sub> per liter medium (results not shown). Absence of O<sub>2</sub> is an absolute prerequisite for the H<sub>2</sub>-production process. The rate of H<sub>2</sub> production in the two samples (Fig. 1, Degassed and Control), measured from the slope of the two lines, was approximately the same, suggesting that the rate of H<sub>2</sub> production is not influenced by the early removal of oxygen from the photobioreactor. However, for the duration of this single batch experiment, initiation of the process occurred sooner and the yield of H2 production was systematically greater in cultures that were degassed than in control ones. This was a direct consequence of the early removal of atmospheric oxygen from the cultures. In conclusion, this experimentation clearly shows that, in a Stage 1 + Stage 2 process in which photosynthetic O<sub>2</sub> evolution and carbon accumulation (Stage 1) alternate with consumption of cellular metabolites and concomitant H<sub>2</sub> production (Stage 2), the effectiveness of the switch from Stage 1 to Stage 2 largely depends on the removal of oxygen from the photobioreactor medium. Thus, future experimental designs seeking to improve the yield of H<sub>2</sub> production in this Two-Stage process need focus on how best to make the transition from aerobic to anaerobic environment in the photobioreactor medium.

### Subtask 2: The research will measure the effect of the pH of the water medium in the burette, to assess the optimal pH conditions for the release of $H_2$ gas in the collection space.

In the Stage 1→Stage 2 process described above, hydrogen gas is generated by the green algae in a 1 L sealed culture. It passes through a volume of water contained in the collection apparatus (beaker and inverted burette) before it can be collected in the gaseous form. Water in the collection apparatus is in equilibrium with atmospheric air. Inevitably, the volume of H<sub>2</sub> gas collected is equal to that produced minus the amount of H2 dissolved in the growth medium of the photobioreactor and in the water of the collection apparatus (beaker and inverted burette). The solubility of molecular hydrogen to degassed water is 0.77 mmoles per liter, and presumably lower in the presence of other gasses (e.g., nitrogen in the photobioreactor; nitrogen and oxygen in the collection apparatus). Moreover, H<sub>2</sub> gas produced photobiologically in Stage 2 is expected to purge other gases from the medium, both in the photobioreactor and in the collection These considerations suggest that there is a complicated and dynamic interaction between the various gases (and the atmosphere) in the collection apparatus, one that might influence the yield of H<sub>2</sub> gas collected. Therefore, experimental conditions that limit the solubility of molecular H<sub>2</sub> in water might help increase the yield of H<sub>2</sub> production in a Stage  $1 \rightarrow$  Stage 2 approach.

**Figure 2** shows the result of a first experimental attempt to influence the  $H_2$  solubility in water. The pH of the water in the collection apparatus was adjusted from the normally neutral (pH=7.0 in Fig. 1) to acidic (pH<2.0 in Fig. 2, solid circles) or basic (pH>12 in Fig. 2, open

circles). The yield and rate of  $H_2$  gas collected were measured under these two different pH conditions. The results shown in Fig. 2 failed to show any significant difference in either rate or yield of  $H_2$  gas collection in the inverted burette as a function of the pH of the medium. These results suggest one of two possibilities: (1)  $H_2$  solubility in water is not an important variable for the determination of yields and rates in  $H_2$  production, or (2) changes of the pH in the  $H_2$  collection apparatus is not the method of choice by which to influence  $H_2$  solubility in water. New insights and experimental designs are needed to conclusively address the question of  $H_2$  solubility in water.

### Task 2. To design and test cell growth media that accentuate the metabolism of $H_2$ production. Effect of salinity on $H_2$ -production

The reversible hydrogenase pathway of electron transport, which leads to the generation of H<sub>2</sub> gas, is thought to function in order to generate ATP energy for the metabolic needs of the cell [Schlegel and Schneider 1978]. If this hypothesis is correct, then, physiological and environmental conditions that require a greater cellular expenditure of ATP may cause a stimulation in the rate of electron transport via the reversible hydrogenase pathway, thereby resulting in greater yields of H<sub>2</sub> gas production. Salinity is an environmental condition that requires expenditure of cellular ATP to prevent accumulation of unwanted Na<sup>+</sup> cations in the cytosol of green algae. Accordingly, the research investigated the yield of H<sub>2</sub> gas production as a function of NaCl concentration in the bioreactor medium. A complete analysis of the Two-Stage process in different salinity concentrations is presented and discussed below.

### Subtask 1: Effect of salinity on chlorophyll content and cell viability.

The Chl content of the cells and the viability of C. reinhardtii were measured as a function of time upon sulfur deprivation in cultures that contained different amounts of NaCl. **Fig. 3** shows that, independent of salinity and as a function of time in the absence of sulfur, the cell density in the culture increased from about  $4x10^6$  cells/mL at 0 h to about  $6x10^6$  cells/mL at 60 h. Subsequently, cell density stayed constant or declined slightly during the 60-100 h period. These result show that no significant loss in cell viability occurs throughout the long sulfur-deprivation stress.

Fig. 3 also shows that the Chl content of the culture increased transiently during the 0.10 h sulfur deprivation period but declined steadily thereafter. After 100 h of sulfur deprivation, only about 50% of Chl content had remained in the cells, suggesting regulated catabolism of some of the Chl-protein complexes in the cell [Melis et al. 2000]. Thus, the Chl content per cell declined from about  $2x10^{-15}$  mol Chl/cell to about  $1x10^{-15}$  mol Chl/cell after 100 h of sulfur deprivation. These results show that some cell division does occur during the first 60 h of sulfur deprivation but that a gradual loss of Chl also occurs during the sulfur deprivation period.

### Subtask 2: Effect of salinity on cellular photosynthesis and respiration.

When *Chlamydomonas reinhardtii* cultures are deprived of inorganic sulfur, the capacity of the cells for  $O_2$  evolution and  $CO_2$  fixation decline significantly with a half-time of about 15-20 h in the light [Wykoff et al. 1998], without a concomitant loss in the capacity of respiration [Melis et al. 2000]. The absolute activity of photosynthesis, measured from the light-saturated rate of  $O_2$  evolution in *C. reinhardtii* (**Fig. 4**, Pmax), declined bi-exponentially from ~120 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> at t=0 h to about 5 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> at t=100 h. Cellular respiration,

measured from the rate of O<sub>2</sub> consumption in the dark (Fig. 3, R), remained fairly constant over the 0·100 h period. It is important to note that the absolute activity of photosynthesis decreased below that of respiration in *C. reinhardtii* after about 25 h of sulfur deprivation. Interestingly, this pattern did not change as a function of salinity, at least in the 0·15 mM NaCl concentration. At higher concentrations, the activity of photosynthesis and the ability of cells to grow were adversely affected [Neale and Melis 1989].

### Subtask 3: Effect of salinity on hydrogen production.

It is known that, sometime after about 25 h of sulfur deprivation, a sealed *Chlamydomonas reinhardtii* culture would quickly become <u>anaerobic in the light</u>, due to the significantly greater rate of respiration than photosynthesis of the cells. This was indeed confirmed by measurements with a Clark-type O<sub>2</sub> electrode (results not shown). Under these conditions, *C. reinhardtii* resorts to the reversible hydrogenase pathway for electron transport, leading to H<sub>2</sub>-production. **Fig. 5** shows results from such measurements with sulfur-deprived cultures of *C. reinhardtii* suspended under different salinity conditions. It is evident that cultures under mild salinity conditions (5 and 10 mM) perform better than the control (0 mM NaCl) and the 15 mM NaCl sample. The optimal concentration of NaCl for maximum H<sub>2</sub>-production was 10 mM. The results show that, at this salinity, the H<sub>2</sub>-production activity of the 10 mM NaCl sample was enhanced, on the order of about 30% in the initial rate and 40% in the yield, compared to that of the control.

These results are consistent with the hypothesis that the reversible hydrogenase pathway serves to drive the formation of ATP energy for the metabolic needs of the cells. They also suggest that further refinement in the design of cell growth media, including the application of mild stress conditions, may lead to further enhancement in the rate constant and yield of  $H_2$ -production by green algae.

### Task 2. To design and test cell growth media that accentuate the metabolism of H<sub>2</sub> production. Effect of ATP biosynthesis uncouplers

The *reversible hydrogenase* pathway of electron transport, which leads to the generation of  $H_2$  gas, is thought to function in order to generate ATP energy for the metabolic needs of the cell. If this hypothesis is correct, then, physiological and environmental conditions that require a greater cellular expenditure of ATP may cause a stimulation in the rate of electron transport via the *reversible hydrogenase* pathway, thereby resulting in greater yields of  $H_2$  gas production. In the previous report, salinity was used as an environmental condition that requires expenditure of cellular ATP to prevent accumulation of unwanted  $Na^+$  cations in the cytosol of green algae (please see January-March 2000 report). In this reporting period, a complementary approach was taken: the ATP generation process was uncoupled from the electron-transport pathway leading to  $H_2$ -production. The goal of this investigation was to see whether such uncoupling might release the "load" and therefore permit greater rates of  $H_2$ -production. Three different classes of such uncouplers were tested and the results are described below for each category.

### Subtask 1: Effect of methylamine-hydrochloride.

Methylamine-hydrochloride acts upon sequestering itself in the interior (lumen) of the photosynthetic membranes. There, it acts by binding protons as the latter are deposited during electron transport. This binding prevents the overaccumulation of protons in the lumen and

alleviates a potentially inhibitory effect it may have in the process of electron transport. In this experimentation, variable amounts (0-50 mM) of methylamine-hydrochloride (CH<sub>3</sub>NH<sub>2</sub>-HCl, pH 7.4) were added to the green algal culture (*Chlamydomonas reinhardtii*) 24 h after sulfur deprivation and immediately prior to sealing of the cultures. Hydrogen accumulation was monitored by the inverted burette method. **Fig. 6** presents a family of curves showing initiation of H<sub>2</sub>-production at about 27 h. In several such experiments, control cultures (Fig. 6, 0 mM) and cultures in the presence of low amounts of methylamine (less than 2 mM) produced H<sub>2</sub> with similar rates and yields. Methylamine concentrations in the 2-7 mM range enhanced the rate and yield, albeit by modest amounts. The initial rate of H<sub>2</sub>-production in the presence of 5 mM methylamine was greater than that of the control by 20-25%. Yields at 96 h were 10-20% better in the presence of 5 mM methylamine than in the control. Thus, the results with methylamine support the notion of enhanced initial rates (by 20-25%) due to the uncoupling of the H<sub>2</sub>-production from the ATP biosynthesis process.

### Subtask 2: Effect of gramicidin.

Gramicidin acts by inserting itself across the lipid bilayer of the photosynthetic membranes, thereby forming channels that permit the efflux of protons from the lumen, as the latter are deposited during electron transport. The unregulated leakage of protons from the lumen has essentially the same effect as that of methylamine, albeit by a different mechanism. **Fig. 7** shows that, qualitatively, gramicidin brings about the same result in terms of hydrogen production as methylamine (Fig. 6). A serious limitation encountered by gramicidin, however, was due to the low solubility of this chemical in the water phase of the growth medium. This constraint limited the use of gramicidin to only low concentrations (up to 5  $\mu$ M). When higher concentrations of gramicidin were injected into the water phase of the growth medium, gramicidin precipitated from the solution in the form of white crystals. Nevertheless, the qualitatively similar results with methylamine and gramicidin support the notion that dissipation of the proton gradient from the interior of the photosynthetic membranes (lumen) to the outside space could enhance the process of electron transport and hydrogen production in green algae.

### Subtask 3: Effect of FCCP.

Carbonyl Cyanide p-Trifluoromethoxyphenyl-hydrazone (FCCP) represents yet another class of ATP biosynthesis inhibitors acting in a mode that does not necessarily involve dissipation of sequestered protons from the chloroplast lumen. Whatever the mode of action of this ATP biosynthesis inhibitor, results in **Fig. 8** show an effect dissimilar to that of the other uncouplers. FCCP appears to only inhibit the rate and yield of  $H_2$ -production. Even low  $\mu M$  quantities had a dramatically inhibitory effect, suggesting that the mode of action of this ATP biosynthesis inhibitor is detrimental to the  $H_2$ -production process. At a concentration of 5  $\mu M$  FCCP, the rate and yield of  $H_2$ -production were lowered by about 80%.

These results strengthen the hypothesis that the reversible hydrogenase pathway serves to drive the formation of ATP energy for the metabolic needs of the cells. Thus, greater expenditure of cellular ATP or uncoupling of the ATP biosynthesis from the electron transport process helps to enhance the rate of H<sub>2</sub>-production. However, these measurements also suggest that use of ATP biosynthesis inhibitors is not the method of choice for the experimental manipulation of H<sub>2</sub>-production, especially under conditions of green algal mass culture. This is due to both the modest effect and the high cost of these chemicals.

### Task 3. Testing the effect of cycling the Stage $1 \rightarrow Stage 2$ process to extend the production of $H_2$ gas by green algal cultures.

Anaerobiosis in C. reinhardtii cultures upon sulfur deprivation. As explained previously, anaerobic incubation of green algae is required to induce the expression of the gene that encodes the reversible hydrogenase and of other genes that are essential for  $H_2$  production. It is also known that  $O_2$  evolved by photosynthesis is sufficient to lower or to fully inhibit the activity of the reversible hydrogenase. This incompatibility between the simultaneous  $O_2$  and  $O_2$  and  $O_3$  production reactions can be overcome upon temporal separation of the two reactions by physiological and fully reversible means. This was achieved upon incubation of the green algae in the absence of sulfur (S)-containing nutrients.

S nutrient deprivation exerts a distinctly differential effect on oxygenic photosynthesis and mitochondrial respiration in green algae. When cultures of the green alga C. reinhardtii are deprived of inorganic S, the light-saturated rates of  $O_2$  evolution and  $CO_2$  fixation decline significantly within 24 h in the light. The absolute activity of photosynthesis, measured from the light-saturated rate of  $O_2$  evolution in C. reinhardtii (Fig. 9), declined bi-exponentially from ~45 mmol  $O_2$  (mol chlorophyll)<sup>-1</sup> s<sup>-1</sup> at t = 0 h to ~2 mmol  $O_2$  (mol chlorophyll)<sup>-1</sup> s<sup>-1</sup> at t = 100 h. The reason for such loss of activity is traced to the requirement of sulfur, needed for the frequent repair of the  $H_2O$ -oxidizing PSII complex. In the absence of sulfur, which is an essential component of cysteine and methionine, protein biosynthesis is impeded and the PSII repair process is blocked.

Cellular respiration, measured from the rate of  $O_2$  consumption in the dark (**Fig. 9**), remained fairly constant at ~13 mmol  $O_2$  (mol chlorophyll)<sup>-1</sup> s<sup>-1</sup> over the 0-50 h period and declined slightly thereafter. It is important to note that the absolute activity of photosynthesis decreased below that of respiration in *C. reinhardtii* after ~22 h of sulfur deprivation.

Sometime after  $\sim$ 22 h of S-deprivation, a sealed *C. reinhardtii* culture is expected to quickly become anaerobic in the light, because of the significantly greater respiratory, than photosynthetic, activity of the cells. In sealed cultures, this leads to **anaerobiosis**, even under saturating illumination. Anaerobiosis is necessary and sufficient to induce the H<sub>2</sub>-production process in green algae.

Photoproduction of H<sub>2</sub> upon S-deprivation in C. reinhardtii. Under conditions of S-deprivation in sealed cultures, i.e., low levels of oxygenic photosynthesis and oxidative phosphorylation, the green alga C. reinhardtii resorts to the production and release of H<sub>2</sub> in order to sustain the electron transport process. Electrons from the residual activity of the H<sub>2</sub>O-oxidizing enzyme and from endogenous substrate pass through the plastoquinone pool, the cytochrome b-f complex and PSI, with electron transport coupled to the reversible hydrogenase pathway. This process results in the release of molecular H<sub>2</sub> and generates ATP energy, which is needed for the maintenance and repair functions of the cell. Figure 10 shows such measurements with S-deprived cultures of C. reinhardtii. Cells in a Roux bottle were incubated in S-deprived media under continuous illumination. Cultures were sealed 24 h after S

deprivation at a time when the rate of photosynthetic  $O_2$  evolution was determined to be equal to, or less than, that of respiration.  $H_2$  gas accumulation was observed in the light (Fig. 10, A) but not in the dark. The rate of  $H_2$  accumulation was constant at ~2.5 ml  $h^1$  for the first 25-35 h before starting to level off. Gas chromatographic analyses of the gas collected showed a ~90%  $H_2$  with the remainder being mostly nitrogen ( $N_2$ ) with traces of  $CO_2$  and  $O_2$ .

The initial rate of  $H_2$  gas accumulation (~2.5 ml  $H_2$  h<sup>-1</sup>), was equivalent to 7 mmol  $H_2$  (mol chlorophyll)<sup>-1</sup> s<sup>-1</sup>. This rate is significantly slower than the capacity of electron transport in the photosynthetic apparatus, which can be estimated from the rate of light-saturated  $O_2$  evolution at the onset of S-deprivation [45 mmol  $O_2$  (mol chlorophyll)<sup>-1</sup> s<sup>-1</sup>; **Fig. 9**]. The estimated  $H_2$  to  $O_2$  ratio ( $H_2:O_2$ , mol:mol) of 0.16:1 suggests a lower than optimal yield of  $H_2$  production vis-a-vis the capacity of the thylakoid membrane for electron transport.

Reversibility and reproducibility of the S-deprivation and/or  $H_2$ -production sequence of events was demonstrated by cycling a single C. reinhardtii culture between the two stages (oxygenic photosynthesis in the presence of S and  $H_2$  production in its absence) for up to three full cycles. **Figure 10** shows the result of such a 'cycling of the stages' in which, at the end of  $H_2$  production in cycle A (**Fig. 10**, **A**), the culture was supplemented with inorganic S (t = 100 h). Addition of inorganic S caused prompt inhibition in  $H_2$  production (**Fig. 10**, beginning of cycle B), due of the ensuing S-induced activation of oxygenic photosynthesis (100 h < t < 130 h). Subsequently, the culture was driven to anaerobiosis upon S deprivation (130 h < t < 160 h) and  $H_2$  production (160 h < t < 220 h). **Figure 10** (**C**) shows a third temporal cycling of the Stage 1  $\rightarrow$  Stage 2 process.

### **CONCLUSION**

The successful Cycling of the Stages, as outlined in this report (Fig. 10), shows that it is possible to extend the production of  $H_2$  gas by a single culture of green algae *ad infinitum* upon alternatively supplementing and depriving the culture of inorganic sulfur. The principle described in this report can be applied to mass cultures of green algae for the sustained production of  $H_2$  gas. This Cycling of the Stages approach would significantly lower the cost of producing  $H_2$  gas commercially as it would alleviate the need of replacing the culture of algae at the end of individual Stage  $1 \rightarrow$  Stage 2 cycles.

Task 3. <u>Testing the effect of supplemental sulfur on the Stage 1  $\rightarrow$  Stage 2 hydrogen production process in green algal cultures.</u>

### Introduction

Hydrogen photo-production upon S-deprivation of green algae cannot be sustained indefinitely. This is because, concomitant with the  $H_2$ -production process, significant catabolism of endogenous substrate occurs (Melis et al. 2000). Endogenous substrate catabolism appears to be essential as it sustains, directly or indirectly, the  $H_2$ -production process. Significant loss of endogenous substrate gradually leads to a slow-down of the rate of  $H_2$ -production. Hydrogen production upon S-deprivation could be sustained, on the average, for only about 5-days before the process was gradually inhibited. At this point, cells must be permitted to go back to normal

photosynthesis in order to replenish needed metabolites before they can be subjected to S-deprivation and  $H_2$ -production for another cycle (please see Progress Report, 30 September 2000).

The present report focuses on the application of limited amounts of sulfur to the growth medium in C. reinhardtii as a way by which to maintain a low-level metabolic activity in the cells and, thus, to possibly prolong the H-production process. This report examines the merit of utilizing micro-amounts of sulfur as a way by which to continuously sustain the  $H_2$ -production process beyond the 5-day limit imposed upon the process by current technology.

### Results

Lack of sulfur from the growth medium brings about a prompt but reversible inhibition of oxygenic photosynthesis. The reason for such inhibition is the apparent chloroplast inability to do high rates of *de novo* protein biosynthesis, needed for the frequent replacement of the D1/32 kD reaction center protein in the H<sub>2</sub>O-oxidizing PSII complex (Mattoo et al. 1987). In the absence of sulfur, which is an essential component of cysteine and methionine, protein biosynthesis is impeded and the PSII repair cycle is blocked (Wykoff et al. 1998). It was of interest to investigate the above phenomenology under conditions of limited sulfur supply. Thus, S-titration of photosynthesis and H<sub>2</sub>-production was undertaken.

**Figure 11** plots the efficiency of PSII primary photochemistry in *C. reinhardtii*, measured from the variable to maximal (Fv/Fmax) fluorescence yield ratio (Kitajima and Butler 1975), as a function of time after transferring the culture from a replete medium to a TAP medium containing variable amounts of sulfur (regulated S-deprivation conditions). In the absence of S (0  $\mu$ M), Fv/Fmax declined exponentially in the light with a half-time of about 17 h, from about Fv/Fmax=0.58 at t = 0 h to about Fv/Fmax=0.08 at t = 60 h. At longer periods of incubation under S-deprivation (t > 60 h), Fv/Fmax remained constant at about the 0.08 level.

In the presence of limited amounts of S (10, 50 and 100  $\mu$ M), there was a lag in the decline of the Fv/Fmax ratio, roughly proportional to the S-concentration used (Fig. 11). The half-times measured for the media containing 10, 50 and 100  $\mu$ M sulfur were 18, 28 and 68 h, respectively. Since care was exercised to eliminate contribution of non-photochemical quenching in the Fv/Fmax ratio measurement (see Materials and methods), the results in Fig. 11 support the notion that S-deprivation interferes with the repair of PSII from the frequently occurring photo-oxidative damage in *C. reinhardtii* (Wykoff et al. 1998, Melis 1999).

The activity of photosynthetic  $H_2O$  oxidation and  $O_2$  evolution also declined with time in S-deprivation. Kinetic patterns of such inhibition showed that, in the absence of S (0  $\mu$ M),  $H_2O$  oxidation activity declined with a half-time of about 13 h (Fig. 12A, P), from about 40 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> at t=0 h, to about 3-4 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> after about 60 h of S-deprivation. Interestingly, photosynthetic  $O_2$  evolution activity appeared to become stabilized at this low-level for times t>60 h (see also Melis et al. 2000, Ghirardi et al. 2000). This is consistent with the Fv/Fmax ratio measurements in Fig. 11, suggesting that a 5-10% of the water oxidizing activity is retained, even after prolonged S-deprivation. When cells were suspended in media with limited amounts of sulfur (10, 50 or 100  $\mu$ M),  $H_2O$  oxidation activity declined with longer half times (15, 22 and 50 h, respectively). The results suggest that, in the presence of even limited amounts of inorganic sulfur, onset of inhibition in PSII activity is delayed. Thus, PSII inhibition appears to depend strictly on sulfur availability. Kinetic patterns of such inhibition were consistent with the S-titration results shown in Fig. 11.

The activity of mitochondrial respiration was not significantly affected by the regimen of S-deprivation (Fig. 12A, R). It declined only gradually as a function of time in S-deprivation from about 12 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> at t=0 h to about 6 mmol  $O_2$  (mol Chl)<sup>-1</sup> s<sup>-1</sup> at t=120 h. The absolute activity of photosynthesis dropped below that of respiration at times that strongly depended on sulfur availability. The incubation time required for this "crossover" point to occur was 23, 27, 36 and 85 h for the samples suspended in the presence of 0, 10, 50 or 100  $\mu$ M S, respectively. Sealed *C. reinhardtii* cultures became anaerobic soon after the crossover point between photosynthesis and respiration (not shown).

Hydrogen gas production and accumulation was detected soon after the establishment of anaerobiosis in the culture, commencing at about 27 h in S-deprivation (Fig. 12B). The rate of  $H_2$ -production was fairly constant at 2.8 ml  $h^1$  during the 27-60 h period. It gradually declined thereafter. The yield and rate of  $H_2$ -production were similar in the 0 and 10  $\mu$ M S samples. In the 50  $\mu$ M S sample,  $H_2$ -production commenced later (at about 40 h) and lasted longer, leading to greater yields. In the 100  $\mu$ M S sample,  $H_2$ -production commenced much later (at times longer than 100 h) and, therefore, did not appear to be promising for the purposes of this application.

### **CONCLUSION**

Pre-calibrated supplemental but limiting amounts of sulfur may boost the yield of hydrogen production in a green algal culture to amounts beyond what has been collected under similar conditions in the total absence of sulfur. Depending of bioreactor geometry and size, such sulfur titration may hold the promise of improving the yield of hydrogen production in this two-stage photosynthesis and hydrogen production method.

### Task 4. <u>Identifying the rate-limiting step in the $H_2$ production process</u>

Given the significant changes in total cellular protein content during H<sub>2</sub>-production in Chlamydomonas reinhardtii (Melis et al. 2000), and in order to gain insight as to the rate limiting step in this process, we focused our attention on the activity and concentration of key photosynthetic proteins. Total cellular protein content was examined upon cell disruption by sonication, followed by protein solubilization and SDS-PAGE analysis. In such experiments, a TAP-grown culture of C. reinhardtii was transferred to TAP-S conditions, and cells were harvested after different periods of sulfur deprivation (0-120 h). Proteins were resolved on the basis of equal Chl loading (4 nmol per lane), as previously described (Zhang et al. 1997). Fig. 13 shows the Coomassie-stained profile of cellular proteins. Notable changes occurred as a function of time in S-deprivation (a) in the composition and amount of the LHC II proteins and (b) in the amount of Rubisco. Both the electrophoretic mobility and the amount of the LHC II apoproteins changed especially at times longer that 60 h in S-deprivation. The amount of Rubisco appeared to decline precipitously as a function of time in S-deprivation (Fig. 14). Two apoproteins, migrating to about 66 kD and 40 kD, respectively, appeared to increase in quantity as a function of S-deprivation. The latter were apparently soluble proteins since examination of an isolated thylakoid membrane fraction from sonicated C. reinhardtii (not shown) did not contain them.

To gain further insight into the various protein changes, specific polyclonal antibodies against the LHC II apoproteins, RbcL subunit, D1 protein of PSII, *psaA/psaB* reaction center

proteins of PSI, and the hydrogenase of *C. reinhardtii* were employed in Western blot analyses of total cell protein extracts. Fig. 14 (LHC II) confirms changes in the composition and amount of the LHC II upon S-deprivation. It is of interest to note that, under the conditions of this experiment, alterations in LHC II were noted only at times t > 60 h, suggesting a threshold for the triggering of these changes. It is also of interest to note that such threshold coincides with the leveling-off of the Fv/Fmax ratio (please see Fig. 11) and of the H<sub>2</sub>O-oxidation activity in the photosynthetic apparatus (Fig. 12) under conditions of S-deprivation. A more detailed analysis of the effect of S-deprivation on the composition and amount of the LHC II was not undertaken in this work.

The Western blot of Fig. 14 (Rubisco) shows a precipitous decline in the amount of this protein as a function of time in S-deprivation. Only traces of this important cellular protein were present at about 48 h of S-deprivation. Within the detection limit of this method, no Rubisco could be detected at times t > 60 h. This result is consistent with the findings of Ferreira and Teixeira (1992) who reported a nearly complete degradation of Rubisco in sulfur-starved *Lemna minor* L. The finding suggests that reductant generated from the residual photosynthetic  $H_2O$  oxidation activity at times t > 48 h is probably not utilized in the Calvin cycle for  $CO_2$  fixation and reduction. Rather, electrons derived upon the residual photosynthetic  $H_2O$  oxidation activity must be channeled exclusively through the hydrogenase pathway and thus quantitatively contribute to the generation of molecular  $H_2$ .

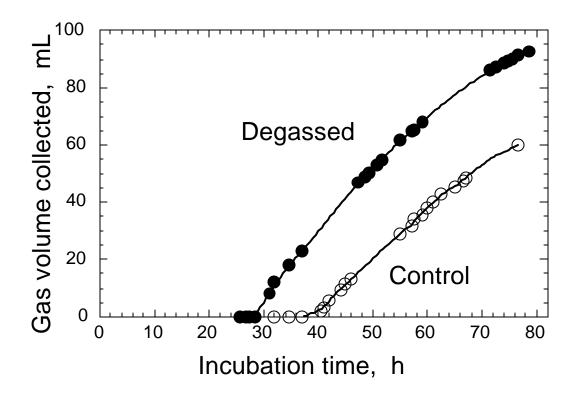
The level of PSII (D1) and PSI (psaA/psaB) reaction center proteins (Fig. 14) declined with time in S-deprivation, consistent with the Q<sub>A</sub> and P700 measurements that were reported earlier (Melis et al. 2000). Interestingly, cross-reaction between an antibody against the hydrogenase (Happe et al. 1994) and a protein band migrating to about 43 kD (Fig. 14, hydrogenase) consistently increased in the 0-60 h S-deprivation period. Rather irreproducible results were obtained at S-deprivation times longer than 60 hours. In some cases, levels of the hydrogenase appeared to decline at times t > 60 h (Fig. 14, hydrogenase, upper panel), whereas, in other cases, the intensity of the cross-reaction gradually increased up to 80 h and declined thereafter (Fig. 14, hydrogenase, lower panel). Moreover, although titer of the immune serum against the hydrogenase was strong (Happe et al. 1994), nevertheless, cross-reaction between the 43 kD band and the antibody was always faint. To overcome this difficulty, gels for the Western blots of the hydrogenase (Fig. 14, Fe-hyd) were loaded with 12 nmol Chl per lane, as opposed to the usual 4 nmol Chl, and the nitrocellulose membranes were exposed to the coloring agents for a longer-than-usual period of time. These observations show that the hydrogenase gene is expressed sparingly under our S-deprivation conditions, thereby limiting the yield of H<sub>2</sub>production under these conditions (Progress Report of 31 December 2000). Fig. 15 shows a quantitative summary of the Western blot results, with the cross-reactions of the various proteins normalized to the maximum (=1.0) detected during the S-deprivation kinetic course.

### **CONCLUSION**

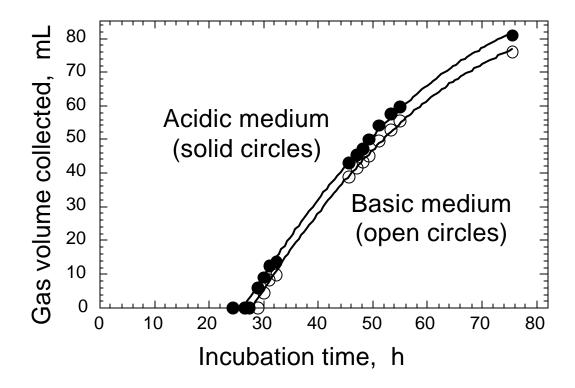
Experimental findings in this work show that the hydrogenase gene (hydA) is expressed sparingly under S-deprivation conditions. This was evidenced by the faint cross-reaction between polyclonal antibodies and hydrogenase in extracts from  $H_2$ -producing cells. The rather low concentration of the hydrogenase is therefore what impedes the rate and yield of  $H_2$ -production under our conditions. To remedy this limitation, genetic

engineering approaches need be applied by which to over-express the hydA gene in order to permit a greater concentration of the hydrogenase enzyme and, therefore, to achieve greater rates of  $H_2$ -production in green algae.

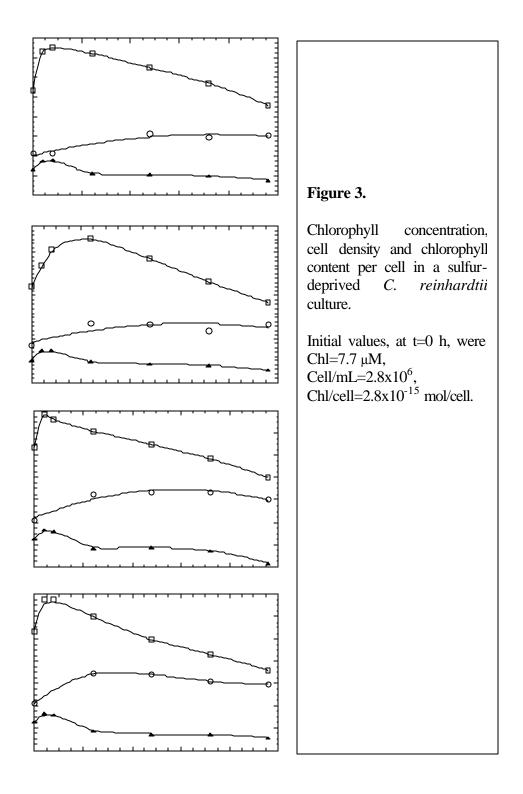
- Reversible application of the switch (presence/absence of S) permits the algae to alternate between O<sub>2</sub> production and H<sub>2</sub> production (temporal separation of the two processes) (Ghirardi et al., 2000), thus bypassing the incompatibility and mutually exclusive nature of the O<sub>2</sub> and H<sub>2</sub> producing reactions.
- Interplay between oxygenic photosynthesis, mitochondrial respiration, catabolism of endogenous substrate, and electron transport via the hydrogenase pathway is essential for this light-mediated H<sub>2</sub>-production process.
- The release of H<sub>2</sub> gas serves to sustain baseline levels of chloroplast and mitochondrial electron transport for the generation of ATP, which is needed for the survival of the organism under sulfur-deprivation stress conditions.

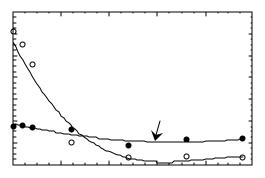


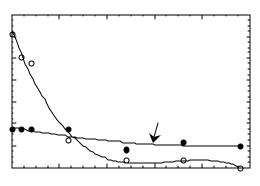
**Figure 1**. Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas reinhardtii*. The culture was sealed at about 25 h after suspension of the cells in a sulfur-free medium with (solid circles) or without (open circles) prior degassing with argon. Values correspond to 1 L culture.

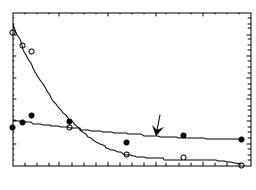


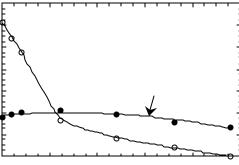
**Figure 2**. Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas* reinhardtii. Cultures were sealed at about 25 h after suspension of the cells in a sulfur-free medium after briefly degassing with argon. pH of the water in the H<sub>2</sub> collection medium (water contained by the beaker and inverted in the inverted burette) was adjusted to an acidic or basic value upon addition of HCl or NaCl (0.1 M final concentration), respectively. Values correspond to 1 L culture.





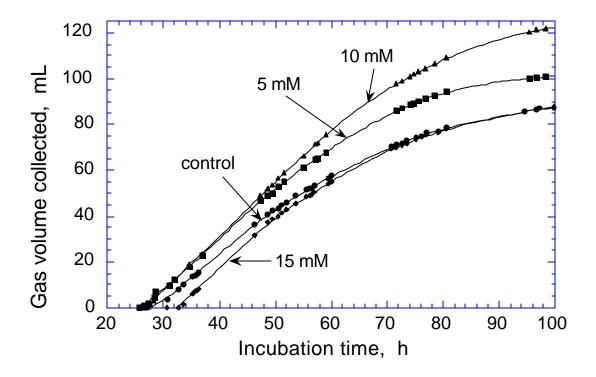






### Figure 4.

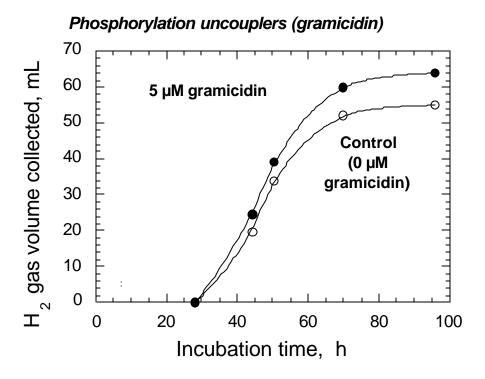
Absolute activity of oxygenic photosynthesis (P) and oxidative respiration (R) in C. reinhardtii cells suspended in a medium devoid of sulfur. Incubation under sulfur-deprived conditions started at 0 h. Cells were suspended in the presence of 10 mM NaHCO<sub>3</sub>, pH 7.6. The rate of cellular respiration (R) was recorded in the dark, followed by a measurement of the rate of light-saturated photosynthesis Rates of photosynthesis (P). were corrected for the rate of dark respiration.



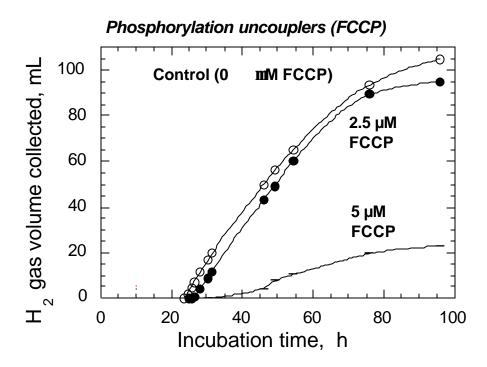
**Figure 5.** Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas reinhardtii*. The culture was sealed at about 25 h after suspension of the cells in a sulfur-free medium. Values correspond to 1 L culture. Gases were collected in inverted burettes by displacement of water. The salinity of the cultures is indicated in mM. Control=0 mM NaCl.

### Phosphorylation uncouplers (methylamine) 120 gas collected, mL 5 mM 100 0 mM CH<sub>3</sub>NH 80 60 2.5 mM 40 10 mM T<sub>2</sub> 20 0 20 40 60 80 100 Incubation time, h

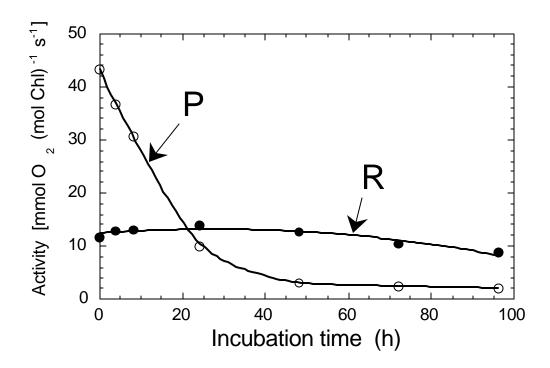
**Figure 6.** Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas reinhardtii*. Values correspond to 1 L culture. Cultures were sealed at about 24 h after suspension of the cells in a sulfur-free medium. Immediately prior to sealing of the cultures, methylamine-hydrochloride was added to the medium (concentration range from 0-10 mM). C=0 mM  $CH_3NH_2$ -HCl. Culture characteristics, at t=0 h, were  $Chl=11~\mu M$ ,  $Cell/mL=4x10^6$ .



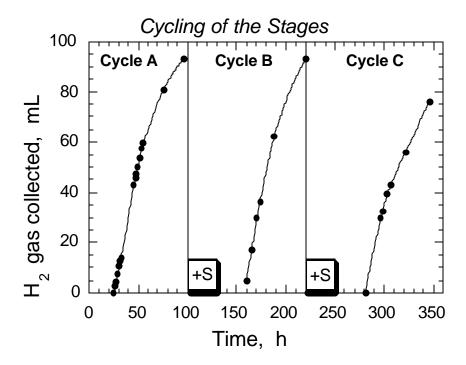
**Figure 7.** Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas* reinhardtii. Values correspond to 1 L culture. Cultures were sealed at about 24 h after suspension of the cells in a sulfur-free medium. Immediately prior to sealing of the cultures, gramicidin was added to the medium (concentration range from 0.5  $\mu$ M). Culture characteristics, at t=0 h, were Chl=7  $\mu$ M, Cell/mL=2.5x10<sup>6</sup>.



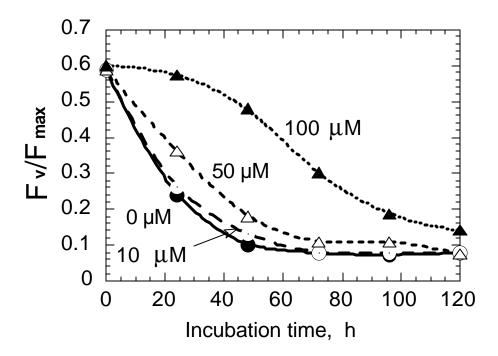
**Figure 8.** Hydrogen gas volume accumulated by displacement of water in an inverted burette as a function of cell incubation time in the absence of sulfur in the green alga *Chlamydomonas* reinhardtii. Values correspond to 1 L culture. Cultures were sealed at about 24 h after suspension of the cells in a sulfur-free medium. Immediately prior to sealing of the cultures, FCCP was added to the medium (concentration range from 0.5  $\mu$ M). Culture characteristics, at t=0 h, were Chl=9  $\mu$ M, Cell/mL=3x10<sup>6</sup>.



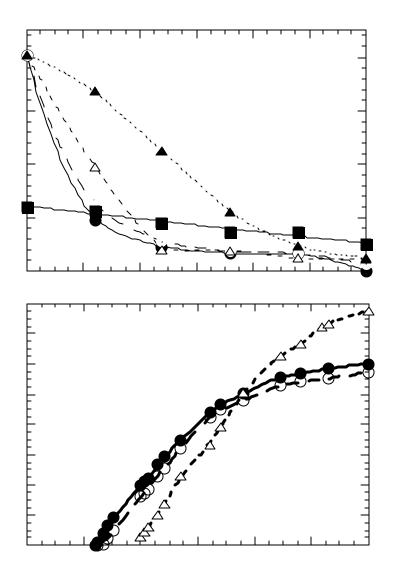
**Figure 9.** Absolute activity of oxygenic photosynthesis (P) and respiration (R) in *Chlamydomonas reinhardtii* strain CC-124 suspended in a medium devoid of sulfur (S). Cells were first grown on Tris-Acetate-Phosphate (TAP) medium. Incubation under S-deprived conditions started at 0 h. The rate of cellular respiration (R) was recorded in the dark, followed by measurement of the light-saturated rate of photosynthesis (P). Rates of photosynthesis were corrected for the rate of dark respiration. Cultures at 0 h contained 2.2 x 10<sup>6</sup> cells ml<sup>-1</sup>.



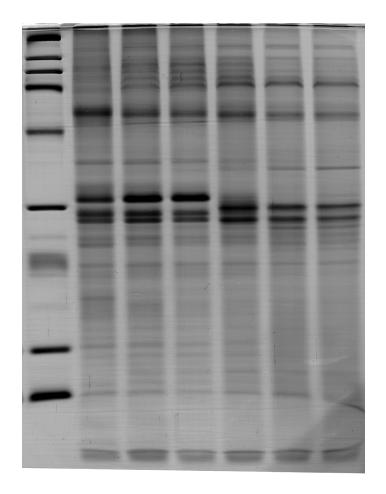
**Figure 10.** Cycling of Stage 1 → Stage 2 oxygenic photosynthesis and H<sub>2</sub> production in *C. reinhardtii*. Cells were suspended in a Roux bottle (850 ml volume) and grown in S-replete media until they reached a density of 2.4 x  $10^6$  cells ml<sup>-1</sup>. They were deprived of inorganic S at t = 0 h and the culture was sealed at t = 24 h. Following H<sub>2</sub>-production in cycle A, the culture was made replete with S (added as sulfate salts in the growth medium to a final concentration of 0.9 mM) strictly during the 100-130 h period. Following H<sub>2</sub>-production in cycle B, the Stage 1 → Stage 2 process was repeated in cycle C (220-350 h).



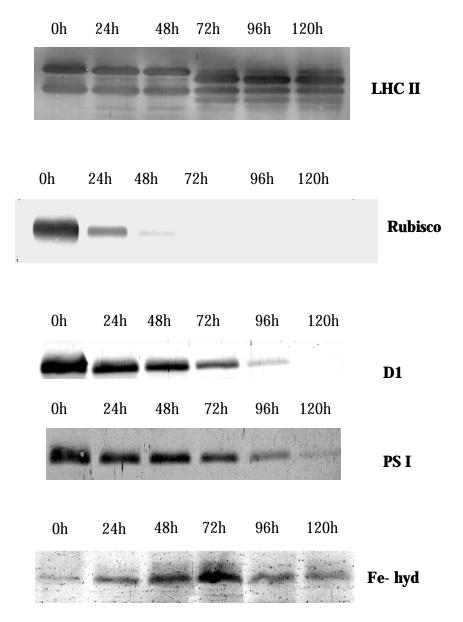
**Fig. 11.** Time-course of the PSII primary photochemical efficiency (Fv/Fmax ratio) in *Chlamydomonas reinhardtii* suspended in a medium of variable inorganic sulfur concentration. Cells were first grown on TAP medium. Incubation under different sulfate concentration (0, 10, 50 and 100  $\mu$ M) conditions started at 0 h. Symbols used: solid circles = 0  $\mu$ M; open circles = 10  $\mu$ M; open triangles = 50  $\mu$ M; solid triangles = 100  $\mu$ M sulfate added at zero hours.



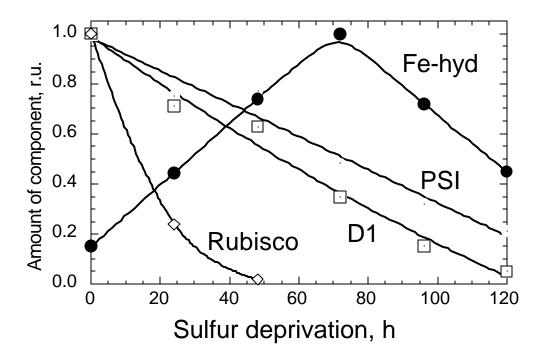
**Fig. 12A,B.** (**A**) Absolute activity of oxygenic photosynthesis (P) and respiration (R) in *C. reinhardtii* suspended in media of variable inorganic sulfur concentration (0, 10, 50 and 100 μM). The rate of cellular respiration (R) was recorded in the dark, followed by measurement of the light-saturated rate of photosynthesis (P). Cultures at 0 h contained  $2.2 \times 10^6$  cell ml<sup>-1</sup>. (**B**) H<sub>2</sub> gas production and accumulation by *C. reinhardtill* cells suspended in media of variable inorganic sulfur concentration. Gases were collected in an inverted burette and measured from the volume of water displacement. Symbols used: solid circles = 0 μM; open circles = 10 μM; open triangles =  $50 \mu$ M; solid triangles =  $100 \mu$ M sulfate added at zero hours.



**Fig. 13.** SDS-PAGE profile of cellular proteins from control (0 h) and S-deprived *C. reinhardtii* (24-120 h). Gels were stained with Coomassie brilliant blue for protein visualization. Note the declining amounts of Rubisco and the altered composition of the LHC II.



**Fig. 14.** Western blot analysis of photosynthetic proteins from *C. reinhardtii*. Nitrocellulose filters were probed with polyclonal antibodies that were specific against the LHC II, Rubisco, D1, *psaA/psaB*, or the hydrogenase. Note the precipitous loss of Rubisco and the transient increase and subsequent gradual decline in the amount of the hydrogenase.



**Fig. 15.** Quantitation of the relative amounts of Rubisco, D1 and *psaA/psaB* proteins in *C. reinhardtii* as a function of time in S-deprivation. Note the precipitous drop in the amount of Rubisco and the more gradual decline in the PSII (D1) and PSI (*psaA/psaB*) reaction center proteins. (**B**) Time course of hydrogenase induction in *C. reinhardtii* as a function of time in S-deprivation. Note the significant differences in the induction and subsequent gradual decline of the hydrogenase between the two different samples.

### **Conclusions, Recommendations and Benefits to California**

### Conclusions

- The research streamlined conditions for H<sub>2</sub>-production under S-deprivation. Thus, improvements in the onset of H<sub>2</sub>-production upon S-deprivation were achieved. Improvements in the yield were modest, on the order og 10-15%.
- Reversible application of the switch (presence/absence of S) permitted the algae to alternate between O<sub>2</sub> production and H<sub>2</sub> production (temporal separation of the two processes), thus bypassing the incompatibility and mutually exclusive nature of the O<sub>2</sub> and H<sub>2</sub> producing reactions. This method will permit the *ad infinitum* albeit intermittent production of H<sub>2</sub> by a green alga culture.
- Interplay between oxygenic photosynthesis, mitochondrial respiration, catabolism of endogenous substrate, and electron transport via the hydrogenase pathway is essential for this light-mediated H<sub>2</sub>-production process.
- The release of H<sub>2</sub> gas serves to sustain baseline levels of chloroplast and mitochondrial electron transport for the generation of ATP, which is needed for the survival of the organism under sulfur-deprivation stress conditions.
- Upon further refinement, the "Two-Stage Photosynthesis and H<sub>2</sub>-Production" process may serve in the generation of H<sub>2</sub> gas for the fuel and chemical industries. Except for the required yield increase, there are no absolute technical barrier for the application of this technology in the commercial production of H<sub>2</sub> gas.

### Recommendations

The "Two-Stage Photosynthesis and  $H_2$ -Production" process brings together two normally separate fields: Energy and Biotechnology. The successful development and employment of this method will boost California's competitiveness in the fields of Energy, Agriculture and Chemistry.

It is thus recommended that every effort be made to advance this technology to its fullest potential

### Benefits to California

Both small-scale (industrial and commercial) and larger (utility) solar energy conversion plants (photobioreactors) can be envisioned utilizing the Two-Stage Photosynthesis and H<sub>2</sub>-Production process. Remote photobioreactors could be installed as modules in arid areas where sunlight is plentiful and alternative uses of land are minimal. Such a process of H<sub>2</sub> gas production would be sustainable, environmentally friendly and economically attractive compared to most other alternatives.

In addition to  $H_2$ , a valuable and clean fuel, the Two-Stage Photosynthesis and  $H_2$ -Production process will generate green algal biomass as a significant "Value-Added Bioproduct" that will enhance the economics and competitiveness of the process. In sum, the process will find application in the:

- Generation of a valuable, clean and renewable fuel.
- Global warming mitigation and reduction in the level of atmospheric polution.
- Production of biomass from which "High-value Bioproducts and Biochemicals" could be extracted.

### Glossary

Chl: chlorophyll -- DCMU: dichlorophenyl dimethyl urea -- FCCP: Carbonyl Cyanide p-Trifluoromethoxyphenyl-hydrazone -- LHC: light harvesting complex -- PMSF: phenymethylsulfonylfluoride -- PSII: photosystem II -- PSI: photosystem I -- PAGE: polyacrylamide gel electrophoresis -- SDS: sodium dodecyl sulfate

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