

Synthesis and Properties of Aluminum Hydride as a Hydrogen Storage Material

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– A Participant in the DOE Metal Hydride Center of Excellence –

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Timeline

- Project start date: FY05
- Project end date: FY09
- Percent complete: *New Project*

Budget

- Expected Total Project Funding:

5 years:	\$3.00M
– DOE Share:	\$2.60M
– Contractor Share:	\$0.40M
- Funding for FY05:
\$200K (DOE),
\$150K (cost share BNL-LDRD)

Barriers

Hydrogen reversibility
Energy penalty of regeneration

Targets

Total system gravimetric : >8%
Total system volumetric : > 0.10 kg H₂/L
Tank operating temp: 85/95°C
Tank operating pressure: 2 bar (30 psig)

Partners

- Participant in DOE Metal-Hydride Center of Excellence; collaborations with MHCoE partners on modeling, regeneration and engineer tank design
- Coordinator of sub-team on aluminum hydride for onboard hydrogen storage systems (U. Hawaii, JPL, SRNL, U. Illinois Carnegie Mellon and SNL)

Mission Statement: To develop and demonstrate a safe and cost-effective light-metal hydride material system that meets or exceeds the DOE goals for on-board hydrogen storage.

Decomposition of AlH_3

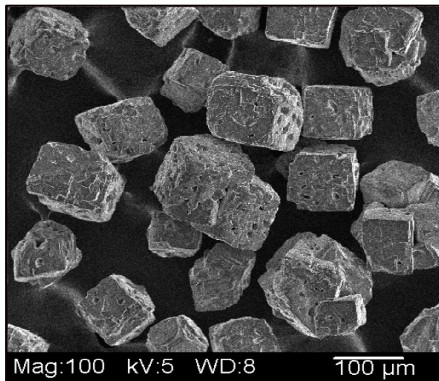


H-capacity (g) = 10.1 wt% (DOE 2010 Storage-Target = 6.0)

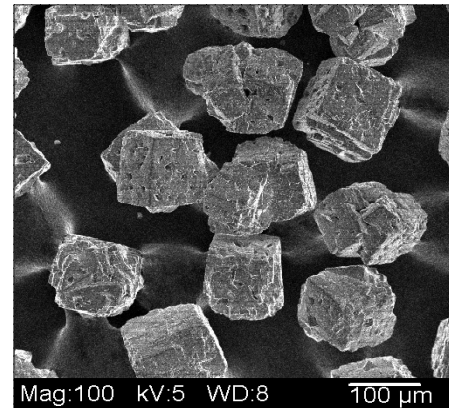
H-capacity (v) = 149 kg/m³ (DOE 2010 Storage-Target = 45)

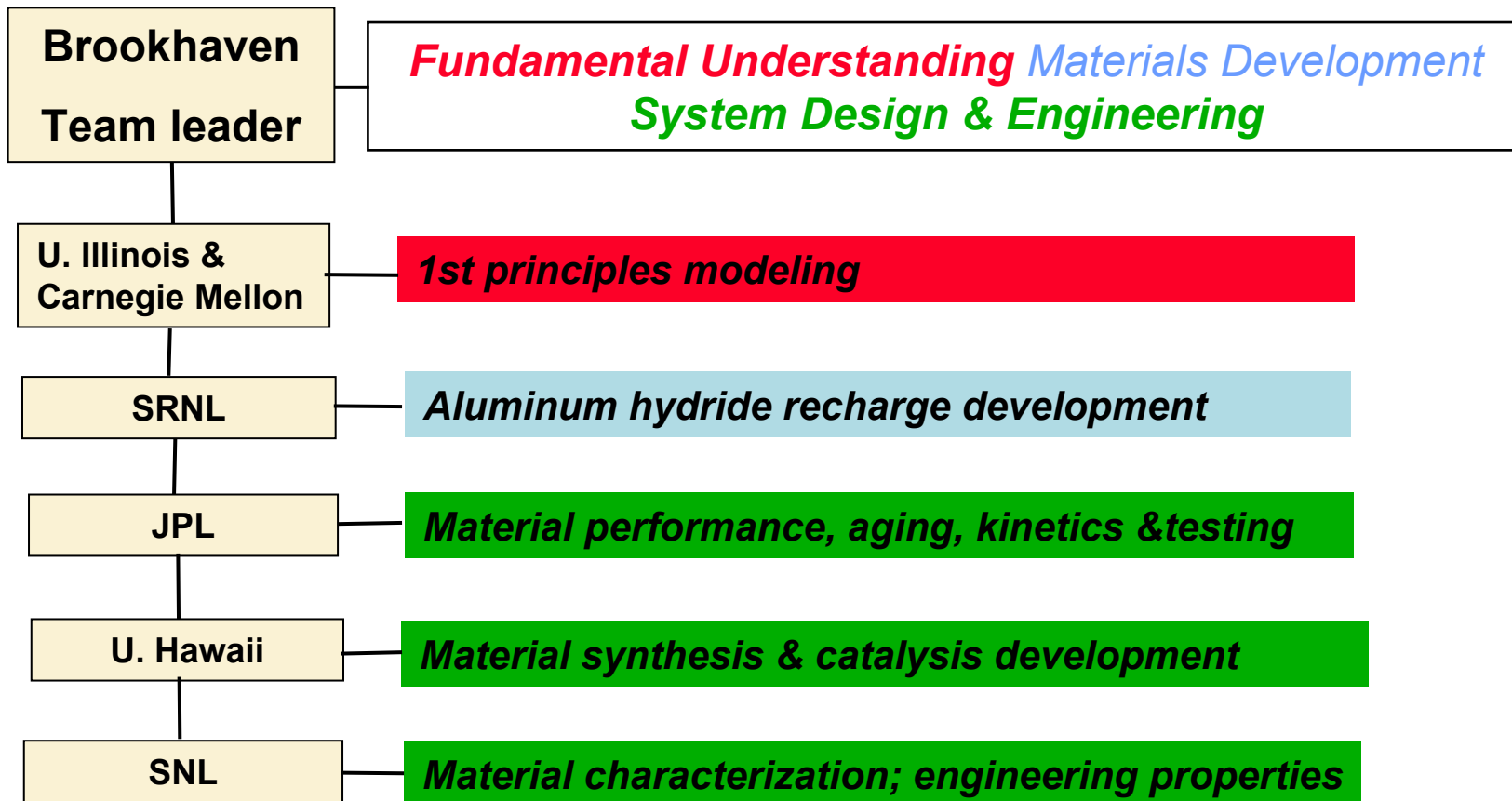
$\Delta H_{\text{des}} = 7.6 \text{ kJ/mol H}_2$ (only 20% of NaAlH_4)

AlH_3

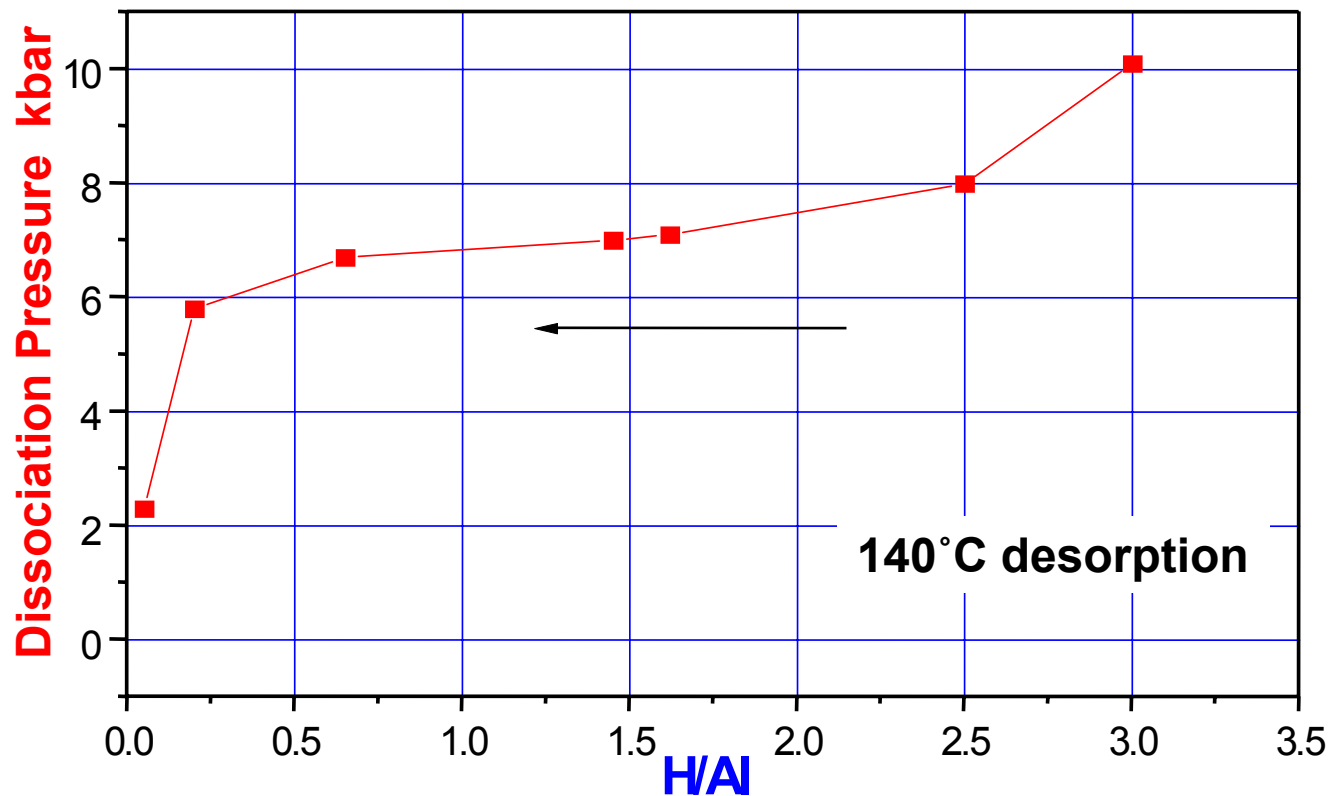


Depleted Al

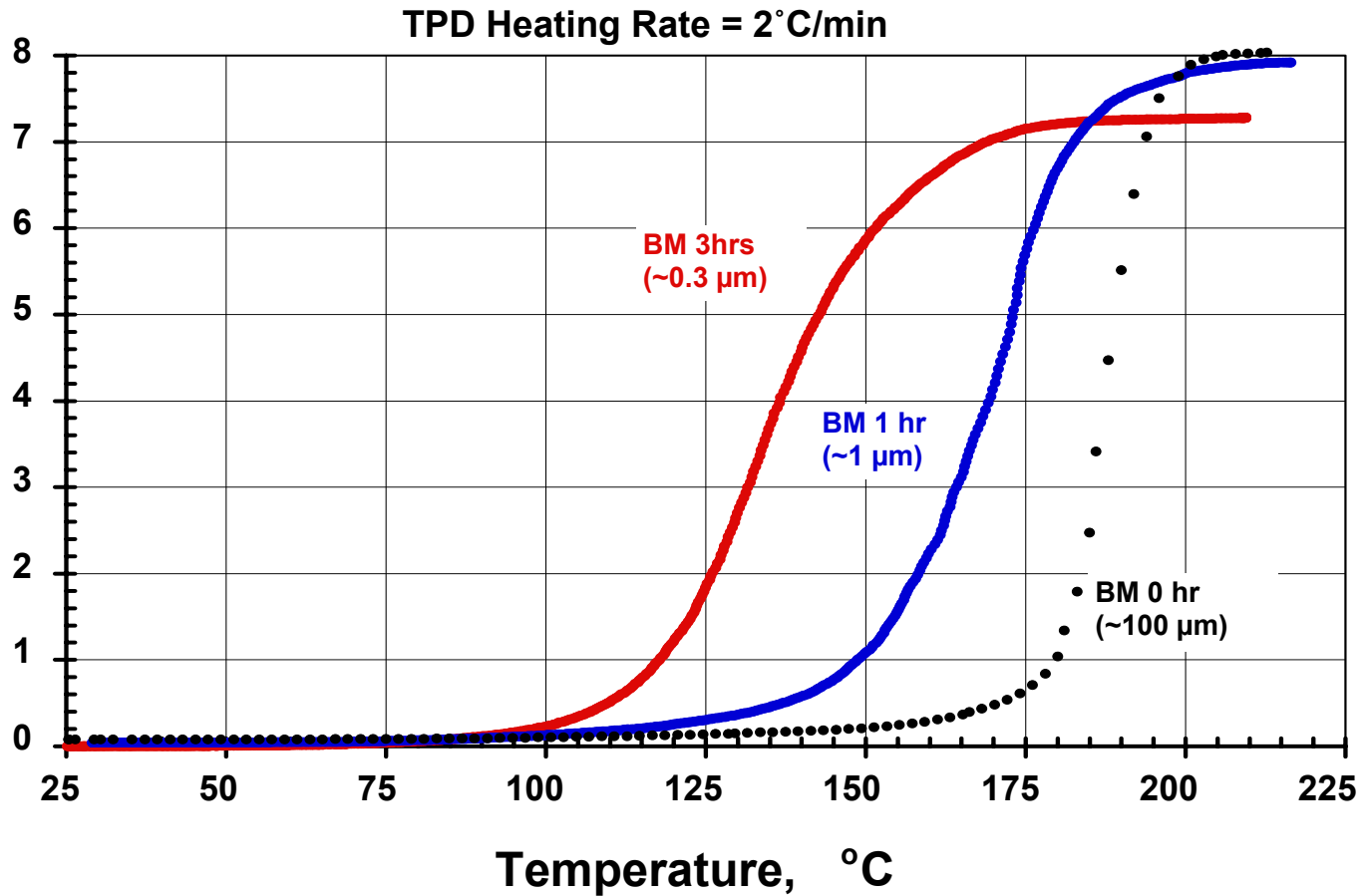




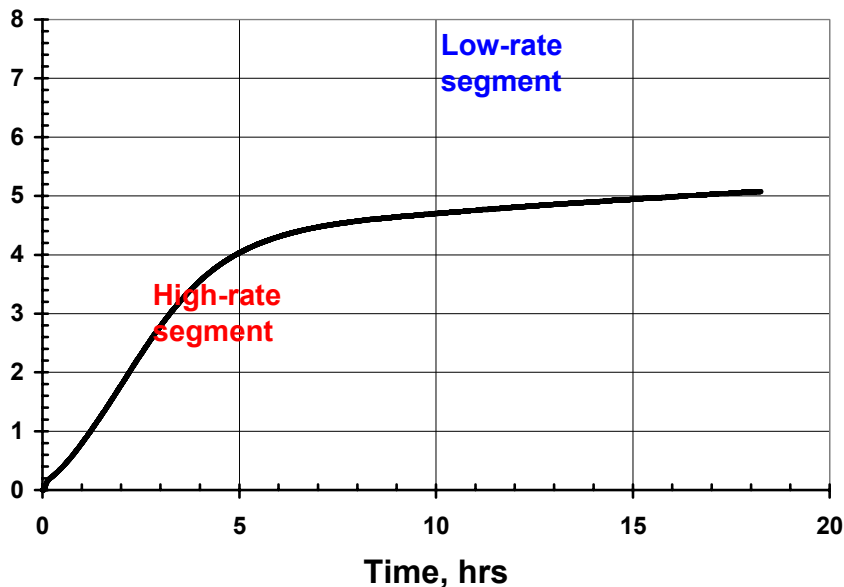
Other partners in MHCoE will also contribute in areas of modeling, simulation and diagnostics



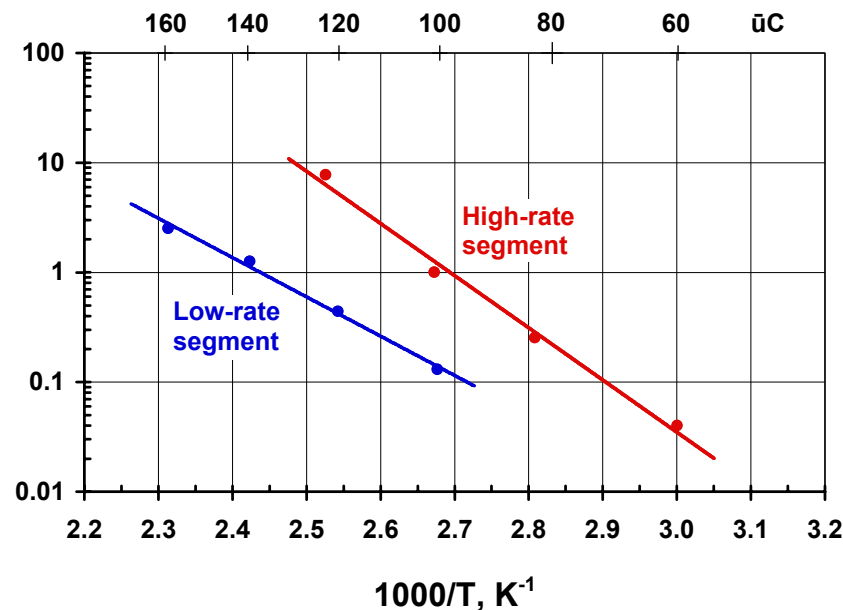
Gas recharging: 28 kbar@300°C !!



100°C



Arrhenius Plot Rate = $k_0 \exp(-Q/RT)$



- high-rate segment: $k_0 = 6.5 \times 10^{12}$ and $Q = 91.3$ kJ/mol H_2
- lower-rate segment : $k_0 = 5.4 \times 10^8$ and $Q = 68.2$ kJ/mol H_2

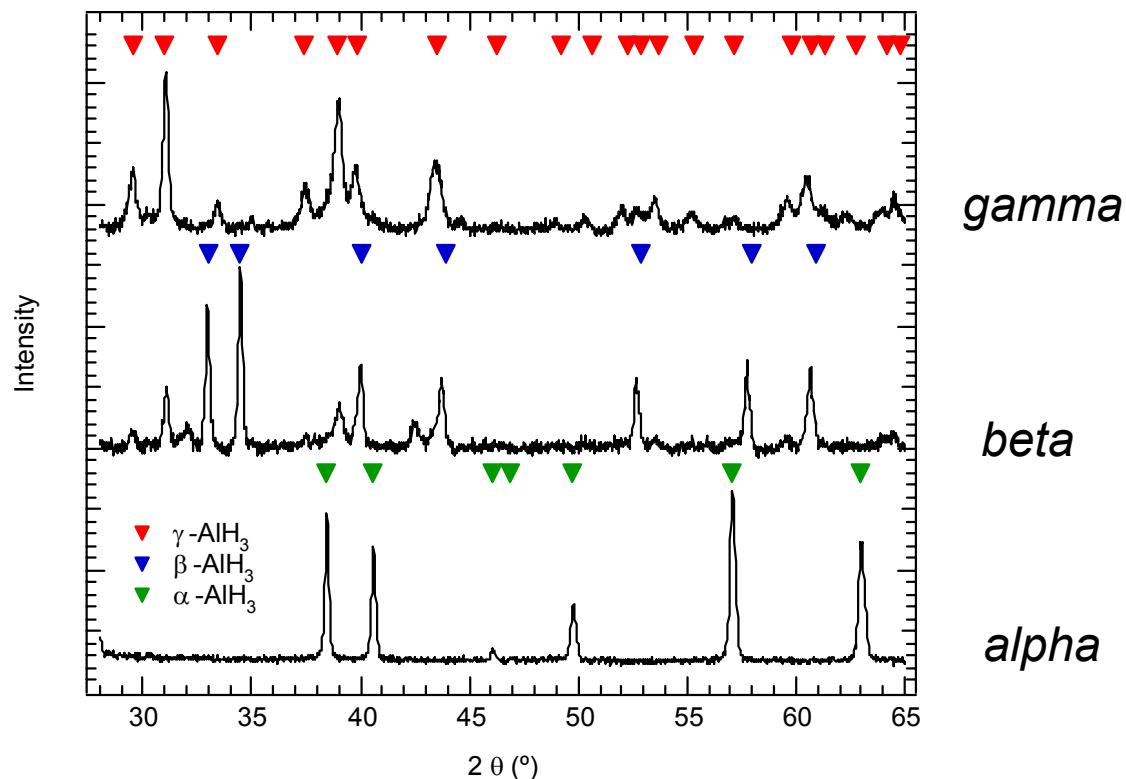
- A total of seven AlH₃ isomers are known to exist:
 - α , α' , β , δ , ε , γ , ζ
- With exception of α -AlH₃, little is known about these polymorphs
- α , β , and γ phases can be grown using an organo-metallic synthesis method



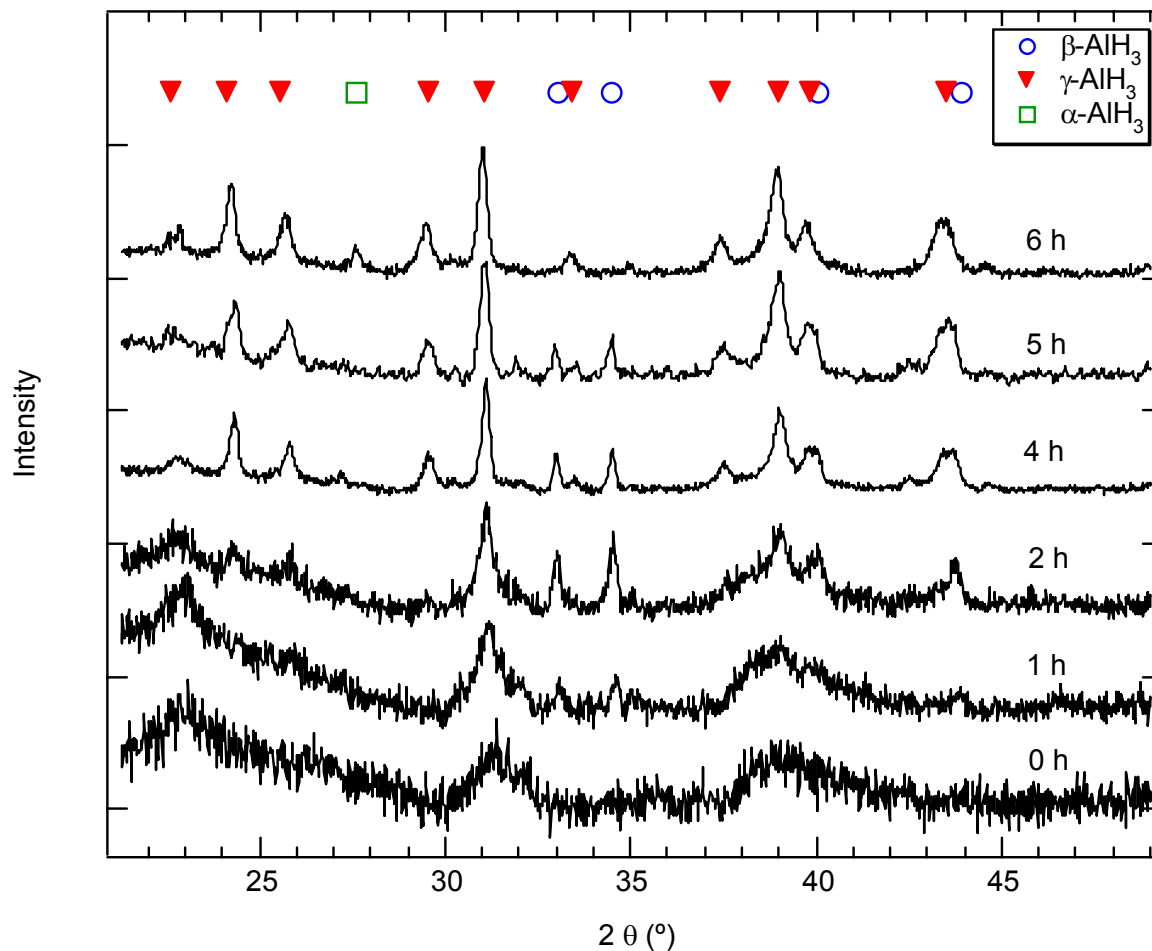
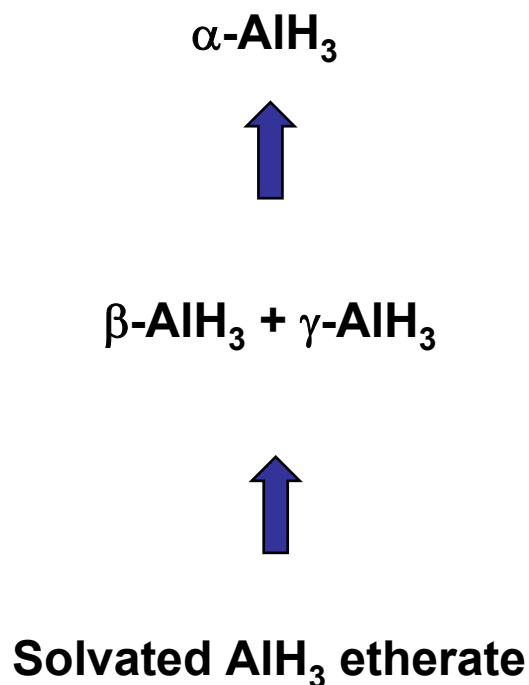
↓ (filter)



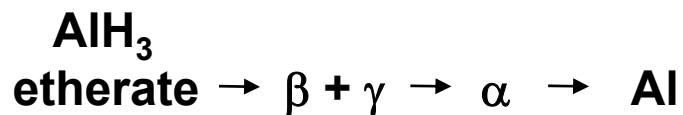
↓ (remove ether)



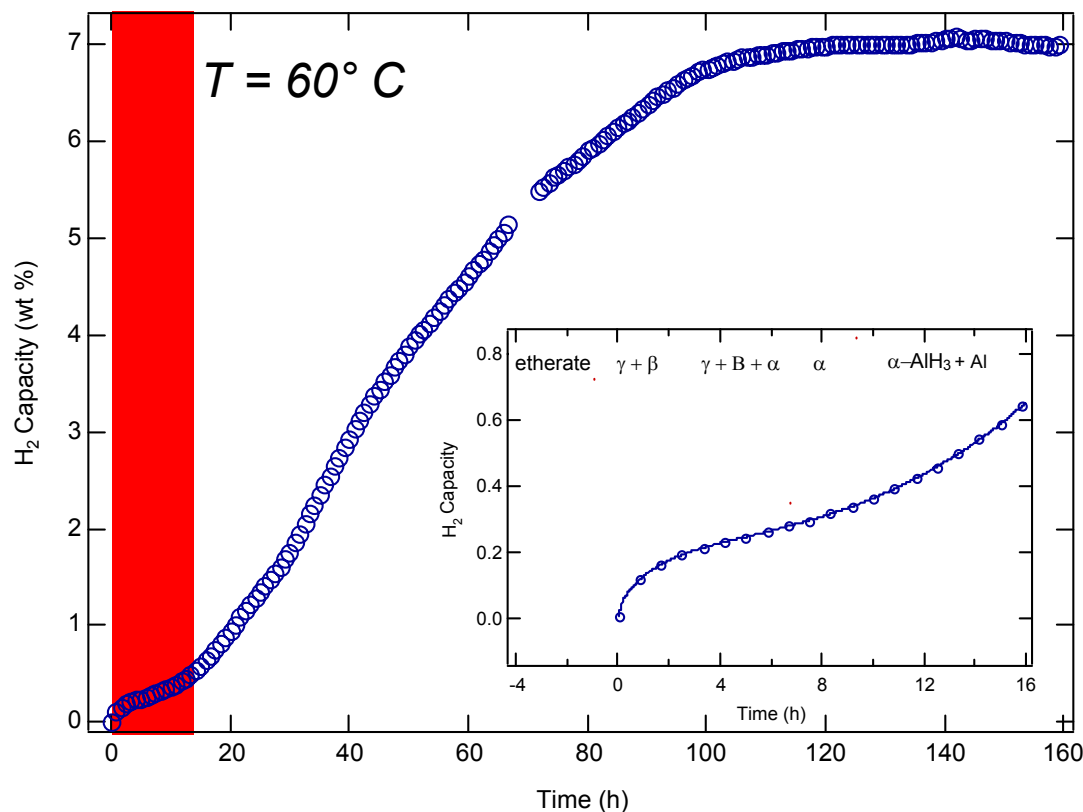
- Ethereal reaction of AlCl₃ and LiAlH₄ yields solvated AlH₃
- Solvent removed by adding excess LiAlH₄ and heating at 60-70° C



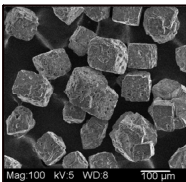
- Desolvated AlH_3 undergoes a number of phase transitions at 60°C



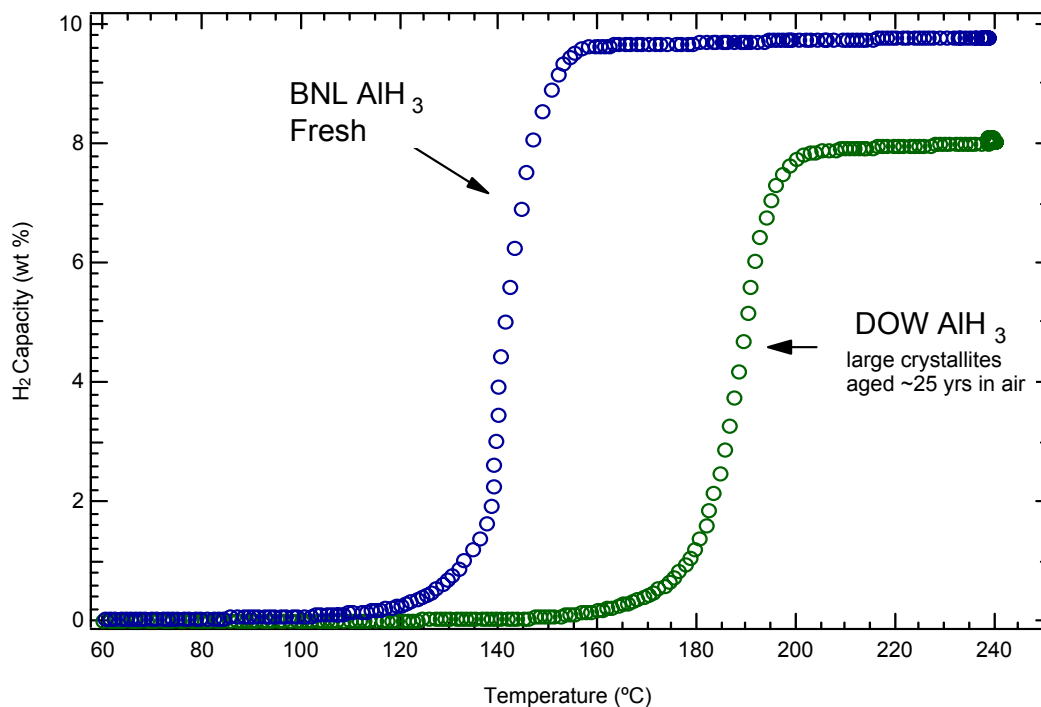
- Transformations occur with little/no H_2 evolution
- AlH_3 decomposition note
induction period ~ 10 h at 60°C



$\gamma\text{-AlH}_3$ and $\beta\text{-AlH}_3$ do not appear to decompose directly to Al and H_2 at 60°C , rather, a transformation to a more stable polymorph ($\alpha\text{-AlH}_3$) occurs first. $\alpha\text{-AlH}_3$ then undergoes complete decomposition to the elements at 60°C ($t \sim 100$ h).



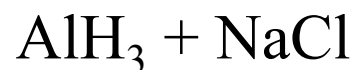
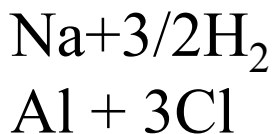
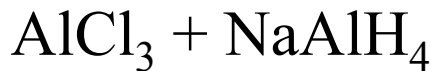
- αAlH_3 synthesized by DOW Chem. Co. composed of large crystallites (50 - 100 μm) aged 25 yrs in air:
 - measure hydrogen capacity 8 wt%
 - onset of rapid H₂ evolution occurs at 160° C
- BNL synthesized AlH_3
 - measured hydrogen capacity ~10 wt%
 - onset of rapid H₂ evolution occurs at 120° C



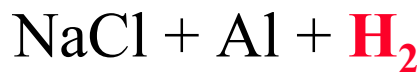
- AlH_3 may be regenerated from recovered products after hydrogen fuel is spent

AlCl_3 prepared by reaction of spent Al with Cl. NaAlH_4 synthesized through reaction of spent Al with $\text{NaH} + \text{H}_2$

AlCl_3 and NaAlH_4 in organic solvent yields AlH_3 and NaCl



NaCl electrolysis to give Na and Cl

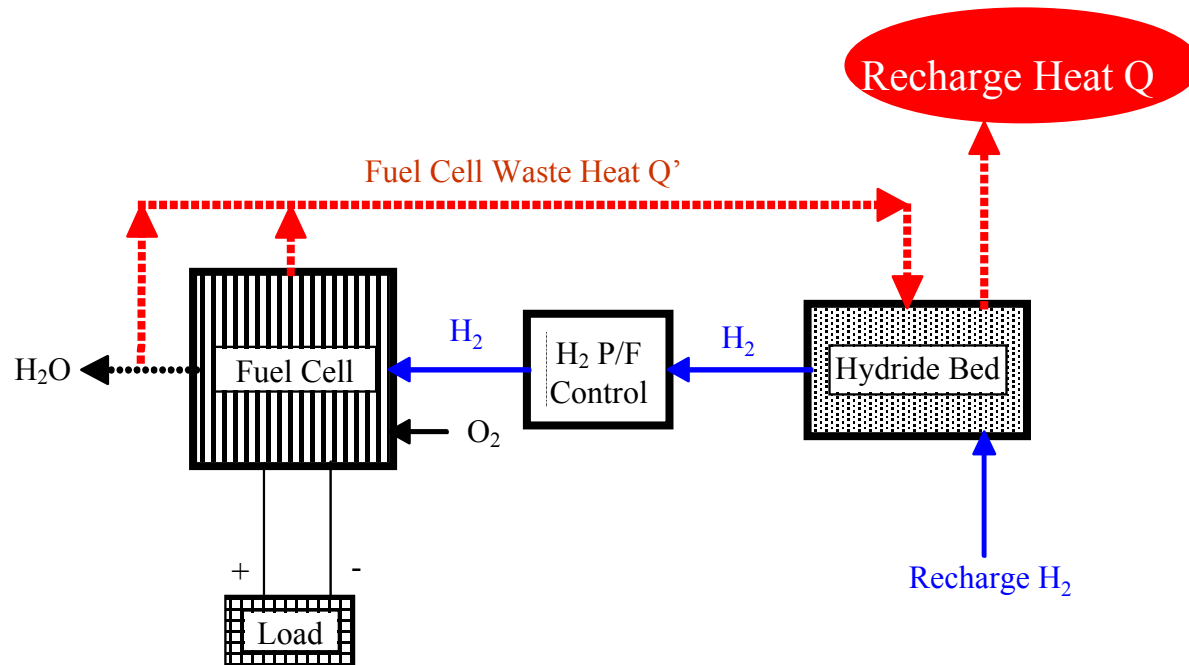


Recycled

NaCl recovered from initial reaction
Al recovered after H_2 fuel is exhausted

Fuel

Note: system is “reversible” since all products are recovered and re-used (except hydrogen).



How much heat must be removed during recharging?

DOE 2010 Target = 3 min = 1.67 kg/min (5 kg H₂ tank)

Take as example NaAlH₄ ($\Delta H = -37$ kJ/mol H₂)

$dQ/dt = 510$ kw or Q total = 91.8MJ !! \Rightarrow Offboard recharge required

Deliverables:

- 10 gm. AlH_3 samples to SwRI; 8% or better by wt. @ 150°C; FY 06
- 10 gm. AlH_3 samples to SwRI; 9% or better by wt. @ 85/95°C; FY07
- 1000 gm AlH_3 samples to SNL for fuel tank development and testing; FY 08

Decision Points:

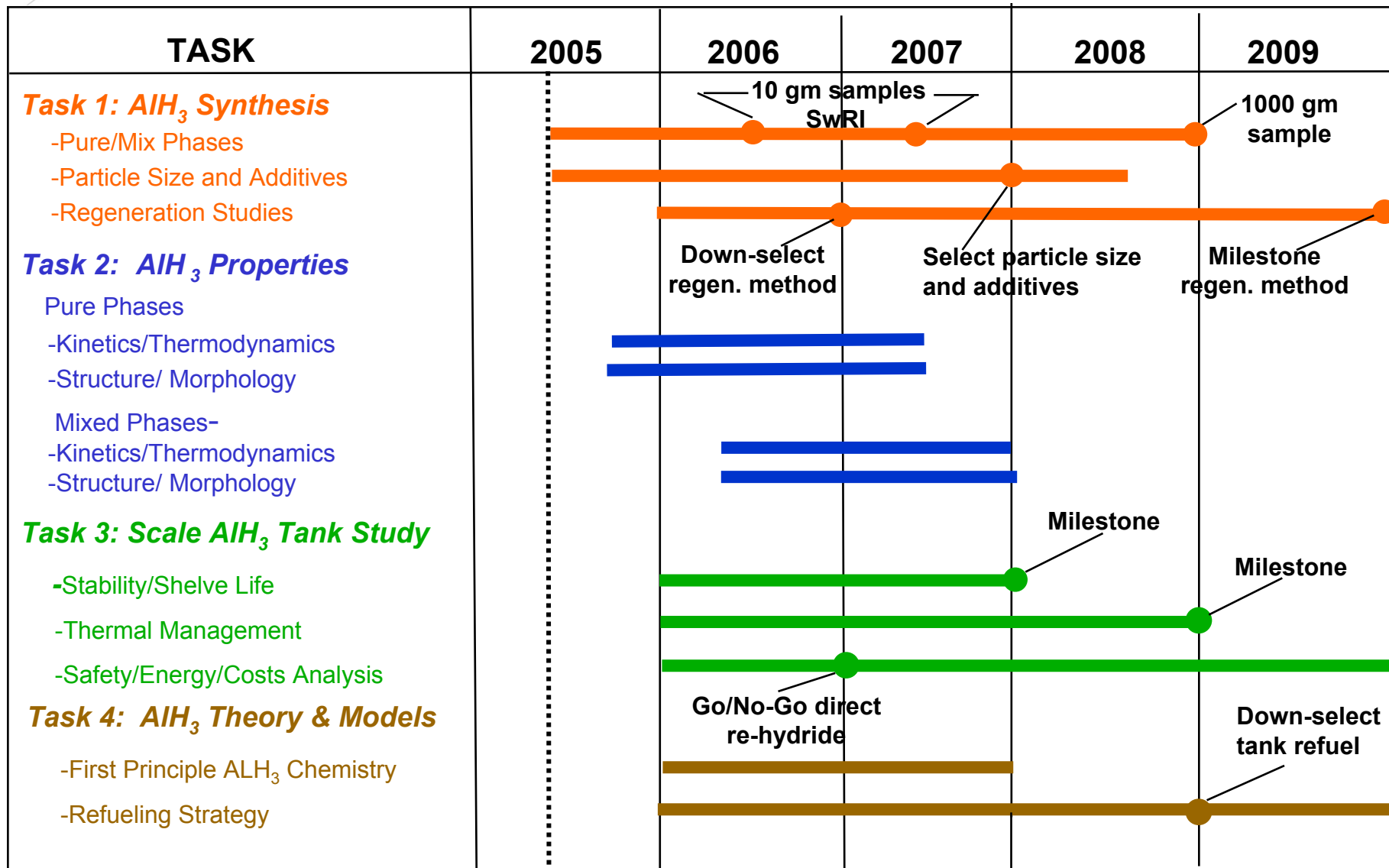
- selection of either direct or chemical method of regeneration; FY 06
- selection of additives and optimum particle size for AlH_3 ; FY 07
- selection of tank refueling method; FY 08

Go/No-Go:

- on the direct onboard re-hydrating of spent aluminum powder; FY 06

Milestones

- complete stability and shelve life studies on AlH_3 ; FY 07
- complete thermal management studies on the control release of H_2 ; FY 08
- selection of method for regenerating AlH_3 ; FY 09



- 1. AlH₃ is a promising H₂ fuel source for a PEM fuel cell due to the high gravimetric/volumetric hydrogen capacity and the low heat required to extract H₂ (7.6 kJ/mol H₂).**
- 2. Doping aged AlH₃ (DOW) with LiH, NaH or KH increases low-temperature decomposition kinetics.**
- 3. α , β and γ AlH₃ have been synthesized at BNL using organo-metallic methods**
- 4. Hydrogen capacities approaching 10 wt% at T < 100° C have been demonstrated with freshly prepared AlH₃**
- 5. Recharging of spent Al back to AlH₃ likely to be done with an offboard process yet to be developed.**