Catalyzed Complex Metal Hydrides

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Abstract

Complex hydrides are mixed ionic—covalent compounds that can serve as reversible H_2 storage media only when they are catalyzed by a transition metal such as Ti. As the prime example, the phenomenology of Ti-catalyzed sodium alanate (NaAlH₄) is reviewed from a historical perspective. Dehydriding yields a theoretical 5.6 wt% H_2 during two-step decomposition, NaAlH₄ \rightarrow Na₃AlH₆ \rightarrow NaH + Al, although 100% recovery of that H_2 is not currently possible. H_2 can be discharged and recharged at practical rates at 125°C. More work is needed on the alanates, in particular, as well as the identification and optimization of the catalytic mechanism and a broad extension of the concept to other than Na-based alanates. The possibility of an even further extension of the concept to other complex hydrides (e.g., the borohydrides and transition-metal complexes) is discussed.

Keywords: hydrogen storage, kinetic properties, metal hydrides.

Introduction

There is a practical need for improved H₂ storage methods with high inherent gravimetric capacity, for example, to carry hydrogen for fuel-cell vehicles. The history and potential of rechargeable metal hydrides for this purpose are presented elsewhere in this issue, clearly showing that we in the hydride field have been hampered by fundamental thermodynamic and kinetic limitations. On the one hand, interstitial hydrides that are easily reversible around room temperature (e.g., those based on V or the AB, AB₂, and AB₅ intermetallic compounds) represent essentially metallic H bonding and are limited to only about 1.5–2.5 wt% reversible gravimetric H capacity. At the other extreme, we have reversible hydrides that exhibit strong covalent or ionic H bonding (e.g., MgH2 and LiH, respectively) that can provide good gravimetric H capacity (7-13 wt%), but unfortunately require temperatures greater than 250°C to release the bound H. This basic dilemma has existed for many years.

Bogdanović et al. suggested a new and different approach, starting in 1996, namely, the use of catalyzed alkali metal alanates, for example, Ti-doped NaAlH₄ and Na₃AlH₆. ^{1,2} Because this approach offers the clear potential of achieving >5 wt% H storage capability at temperatures that are only modestly greater than ambient (e.g., 50–100°C), past thermodynamic barriers were considered to be breached. Early

work at the Max-Planck-Institut für Kohlenforschung in Mülheim, Germany (MPI—Mülheim), was quickly confirmed by other investigators and has resulted in the generation of a great deal of worldwide interest (both fundamental and practical) over the past five years. It is our purpose here to briefly review the fundamentals of the catalyzed alanates and the recent practical progress made and then to comment on the need for future research and development in this area. In particular, we will suggest that the catalyzed alanate complex hydrides may have more general applicability to other complex hydrides. We do not cover here the aqueous complex hydride solutions (e.g., NaBH₄) that are catalytically hydrolyzed to generate H₂ gas.³

Chemistry and Thermodynamics of NaAIH₄ and Na₃AIH₆

The NaAlH₄ and Na₃AlH₆ mixed ionic-covalent complex hydrides have been known for many years. As shown schematically in Figure 1, NaAlH₄, for example, consists of a Na¹⁺ cation and a covalently bonded [AlH₄]¹⁻ complex. In the case of Na₃AlH₆, there is a related [AlH₆]³⁻ complex. These alanates have been synthesized by both indirect and direct methods and used as chemical reagents (see Reference 2 for a historical review of alanate synthesis). However, the practical key to

using the Na alanates for hydrogen storage is to be able to easily accomplish the following reversible two-step dry-gas reaction:

$$NaAIH4 \rightleftharpoons 1/3Na3AIH6 + 2/3AI + H2$$

$$\rightleftharpoons NaH + AI + 3/2H2.$$
(1)

Stoichiometrically, the first step consists of 3.7 wt% H₂ release, and the second step 1.9 wt% H₂ release, for a theoretical net reaction of 5.6 wt% reversible gravimetric H storage. Although Dymova et al. showed that the reversibility of Reaction 1 was possible,^{4,5} the conditions required were impractical in their severity. For example, the formation of NaAlH₄ from the elements required temperatures of 200-400°C (i.e., above the 183°C melting point of the tetrahydride) and H₂ pressures of 100–400 atm. Fortunately, the addition of a Ti catalyst makes the reversibility of Reaction 1 profoundly easier, as we shall show, and thus much more practical for H storage.

The thermodynamics of Reaction 1 are classic and comparable with many other metallic, ionic, and covalent hydrides. As shown in Figure 2, typical low-hysteresis, two-plateau absorption and desorption isotherms can be measured. Temperature dependencies of the plateau pressures *P* are related to the van't Hoff equation

$$\ln P = \Delta H / RT - \Delta S / R, \tag{2}$$

where ΔS is the entropy change, R is the gas constant, and the enthalpy changes ΔH for the NaAlH₄ and Na₃AlH₆ decompositions are about 37 kJ/mol H₂ and 47 kJ/mol H₂, respectively. This allows the direct comparison of the Na-alanate thermodynamic properties with those of other typical hydrides by means of the van't Hoff diagram of Figure 3. We see that NaAlH₄ has thermodynamics comparable to those of classic low-temperature (LT) hydrides LaNi₅H₆ and TiFeĤ—that is, in the range useful for a near-ambient-temperature hydrogen store. Na₃AlH₆ requires about 110°C for H₂ liberation at atmospheric pressure and is therefore less convenient

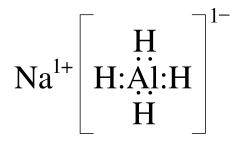


Figure 1. Schematic formula for NaAlH₄.

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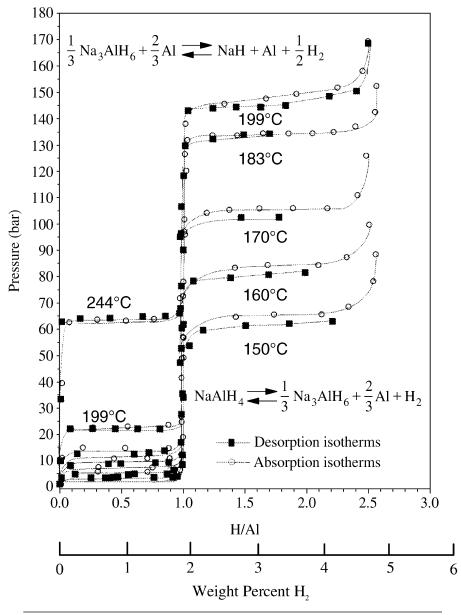


Figure 2. Pressure-composition isotherms for NaAlH₄ and Na₃AlH₆.²

for, say, supplying a fuel cell that provides waste heat ($<80^{\circ}$ C) that is not suitable for supplying the required enthalpy of H_2 desorption. On the other hand, the Na_3AlH_6 van't Hoff line falls between the LT intermetallic hydrides and the high-temperature (HT) Mg and Mg-alloy hydrides, thus filling a moderate-temperature (MT) gap that might be useful for non-fuel storage applications such as heat pumping and heat storage.²

The Importance of Catalysis

The practical use of Reaction 1 requires catalysis for achieving good kinetics. Our first work on catalyzed alanates at MPI—

Mülheim was derived from studies that used transition-metal catalysts for the preparation of MgH₂. We doped NaAlH₄ with Ti by solution-chemistry techniques whereby nonaqueous liquid solutions or suspensions of NaAlH₄ and either TiCl₃ or the alkoxide Ti(OBuⁿ)₄ [titanium(IV) n-butoxide] catalyst precursors were decomposed to precipitate solid Ti-doped NaAlH₄.^{1,2} An alternate approach was taken by Jensen et al. and Zidan et al. at the University of Hawaii, whereby the liquid Ti(OBuⁿ)₄ precursor was simply ballmilled with the solid NaAlH₄.6,7 They also added Zr(OPrⁱ)₄ (where Prⁱ indicates the isopropyl group) to help stimulate the kinetics of the second step (Na₃AlH₆ decomposition) of Reaction 1. Zaluska et al. also obtained positive results by ball-milling with carbon (i.e., not using a transition-metal catalyst). Ball-milling with alkoxide catalyst precursors does result in *in situ* decomposition during at least the first several hydriding/dehydriding cycles, resulting in significant contamination of the H₂ with hydrocarbons; using the inorganic TiCl₃ catalyst precursor is clearly better if one wishes to use the ball-milling catalyst-doping approach. More detailed reviews of the recent history of catalyzed alanate work are available. 10,11

The dramatic effects of Ti catalyst level (using the dry TiCl₃-NaAlH₄ ball-milling/ doping technique¹²) on 125°C hydriding kinetics and capacity are shown in the hydriding curves of Figure 4. The kinetics are dramatically increased and capacity decreased with increasing catalyst level. Nearly identical catalyst effects are seen with desorption experiments, although the two steps of Reaction 1 are more clearly sequential in desorption. 12,13 So, it is very clear that catalysis affects both of the reaction directions of Reaction 1 as well as both steps. The capacity is decreased with increasing catalyst level because the catalyst precursor reacts with some of the Na as part of its process to produce the catalyst itself:12

$$(1 - x)$$
NaAlH₄ + x TiCl₃ \rightarrow
 $(1 - 4x)$ NaAlH₄ + $3x$ NaCl + x Ti
+ $3x$ Al + $6x$ H₂. (3)

Reaction 3 is at least partly hypothetical. It is clear from x-ray diffraction (XRD) studies that the Cl does react with the Na component of the alanate to form NaCl, 13 but the final form of the Ti catalyst is not clear.14 We think it is probably metallic, as shown, but rather than being elemental, it may be in the form of an alloy or intermetallic compound (e.g., with Al). Another possibility, recently suggested from latticeparameter studies, is that the transitionmetal dopant (e.g., Ti) actually acts not as a classic surface "catalyst" on NaAlH₄, but rather enters the entire Na+ sublattice as a variable valence species to produce vacancies and lattice distortions, thus aiding the necessary short-range diffusion of Na and Al atoms. 15 Ti, derived from the decomposition of TiCl₄ during ball milling, seems to also promote the decomposition of LiAlH₄ and the release of H₂.¹⁶

In order to understand the role of the catalyst, Sandrock et al. have performed detailed desorption-kinetics studies (forward reactions, both steps, of Reaction 1) as a function of temperature and catalyst

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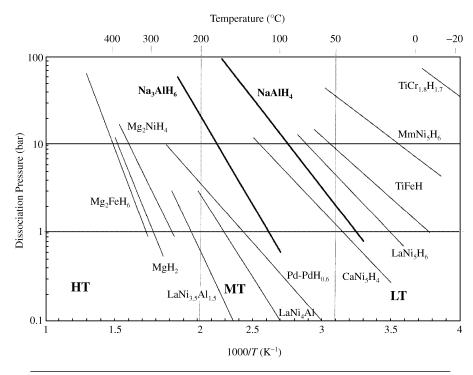


Figure 3. A van't Hoff diagram comparing NaAlH $_4$ and Na $_3$ AlH $_6$ dissociation pressures with those of other well-known hydrides. HT, MT, and LT stand for high-, medium-, and low-temperature hydrides, respectively. Mm in MmNi $_5$ H $_6$ is misch metal, a low-cost mixture of rare-earth elements.

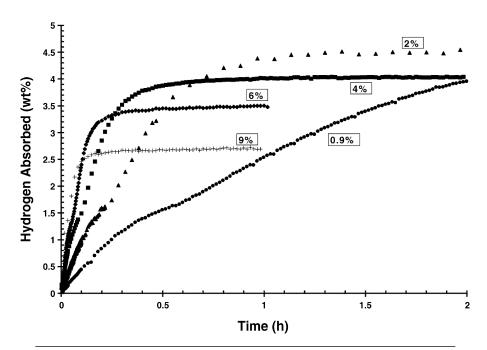


Figure 4. H_2 absorption curves starting from NaH + Al (dehydrided NaAlH₄), as a function of added TiCl₃ catalyst precursor (expressed in mol%). Initial temperature $T_i = 125^{\circ}C$. Applied hydrogen pressure $P_{H_2} = 81-90$ atm. ¹²

level. ¹² Both the NaAlH₄ and Na₃AlH₆ decomposition reactions obey classic, thermally activated behavior consistent with the Arrhenius equation

Rate =
$$k \exp(-Q/RT)$$
, (4)

where k is the pre-exponential rate constant and Q is the activation energy. For example, the Arrhenius plots for undoped and 4 mol% Ti-doped Na alanate are shown in Figure 5. Catalysis results in multiple order-of-magnitude increases in kinetics for both reactions. This important practical result of catalysis is a combined result of both changes in slopes (Q) and intercepts (k) of the Arrhenius lines. If one plots the activation energy Q as a function of catalyst loading, as shown in Figure 6, it is very clear that the smallest Ti addition (0.9 mol%) has marked effects on lowering Q for both steps of Reaction 1. However, further increases in Ti level have no effects, at least not on Q. The dramatic decrease in Q indicates a major discontinuous change in the thermally activated mechanism. Further increases in desorption kinetics accrue with further increases in Ti level, but only through increases in the preexponential rate constant k.12

Work Yet Needed on the Alanates

It has been an interesting and exciting five years since the first publication showing the potential for catalyzed NaAlH4 and Na₃AlH₆.¹ Data generated on these materials thus far show levels of NaAlH4 charging and discharging rates that approach practical viability at temperatures suitable for fuel-cell vehicles and other applications. The Na₃AlH₆ decomposition rates and temperatures are not quite adequate yet. But most would agree that the practical possibilities for a new lowtemperature generation of 5 wt% hydrides have been shown with this class of materials. But there is much yet to do. We herewith summarize our opinions on the R&D and engineering activities yet needed.

Identity and Mechanism of the Ti Catalyst

We do not yet know the identity of the effective catalyst, nor how it works in such a dramatic manner. XRD and microscopic analyses have not led to its identification, probably because it is amorphous, too fine, ^{13,14} or is substitutionally located in the alanate lattice itself. ^{15,16} Our own attempts to mechanically blend various hypothetical catalyst species have failed. Can we produce effective catalysts only by the *in situ* decomposition of a precursor? How does the catalyst really work to ease the thermal activation process? We need to

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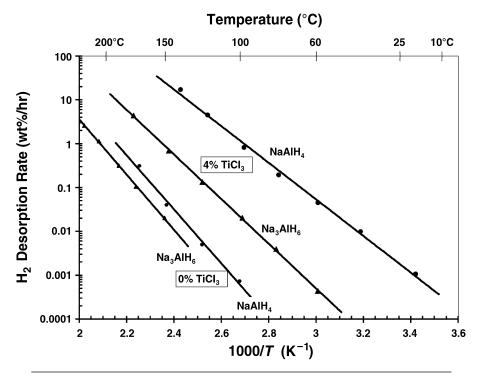


Figure 5. Arrhenius lines for NaAlH $_4$ and Na $_3$ AlH $_6$ decompositions for 0 mol% and 4 mol% added catalyst precursor TiCl $_3$.¹²

answer such key questions if we are to effectively perform the next step, the full optimization of the catalyst.

Optimization of the Catalyst

Most catalyst work thus far has concentrated on the transition metals Ti, Zr, and Fe, along with the nonmetal carbon. Surely we have not optimized the catalyst through these limited investigations. What is the best catalyst for NaAlH₄? Is there something better than Ti? Is there something better than Ti or Zr for the problematic Na₃AlH₆ decomposition?

Hydrogen Capacity and Cyclic Retention

To our knowledge, no one has practically achieved the full cyclic potential of NaAlH₄. For example, see Figure 2, which shows that the full capacity of Reaction 1 $[\Delta H/A]$ (the change in hydrogen content relative to a fixed amount of Al) = 3, or $\Delta wt\% = 5.6$] is not quite achieved. Either initial H capacities are low,8,9,12 or the full capacity is lost after the first cycle by not achieving the full NaAlH4 stoichiometry during charging.² Part of the loss is clearly associated with the catalysis process itself (e.g., Reaction 3), but that is not the whole story. We need more cyclic data, along with associated metallography and other analytical techniques, to see what is physically and chemically happening during cycling.

Engineering Data

Early attempts to look at larger alanate beds from an engineering point of view originated at Sandia National Laboratories9 and are continuing there and at other laboratories. These results are very preliminary and not necessarily focused on the final and optimum catalyzed material. Like the extensive work done on LT intermetallic hydride beds, we need to learn how to put the alanates into practical, safe configurations. We need to know thermal conductivities and expansion behavior. We need to know if there are potential reactions with container materials. The alanates are well known for their reactivity with water, but we need to carefully quantify water reactivity, pyrophoricity, and other aspects of safety.

Thermodynamic Tailoring of Alanates

The history of intermetallic hydrides is deeply laced with thermodynamic tailoring by means of partial substitution of secondary and higher-order components (see the article by Bowman and Fultz in this issue). Are there such possibilities for the alanates? We know that Li can be partially substituted for Na in NaAlH₄, ^{1,2} but

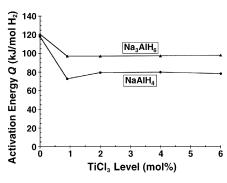


Figure 6. Activation energies Q for NaAlH₄ and Na₃AlH₆ decompositions as a function of added TiCl₃.¹²

are there other possibilities? Numerous $M(AlH_4)_x$ species are known,¹⁷ but their thermodynamic stabilities are largely unknown in more than a qualitative sense. In pure states, which will respond to catalysis? Which can be used for thermodynamic tailoring of NaAlH₄, for example? Is there something that will selectively increase the Na₃AlH₆ plateau pressure without affecting the NaAlH₄ plateau pressure or overall H capacity?

Improved Synthesis and Catalyzing Methods

The alanates would seem to have the potential for low cost. In principal, Na and Al are cheap. But NaAlH $_4$ has been made (by direct synthesis) and sold in commercial quantities at rather high cost (\$40–50/kg). If our desired end product is a catalyzed alanate, are there combinations of synthesis and catalysis that will make the alanates cheaper than in the past? For example, recent attempts to directly synthesize catalyzed NaAlH $_4$ from powder mixtures of NaH + Al + catalyst precursor $_{18-20}^{18-20}$ seem very promising and deserve more attention.

Extension to Other Complex Hydrides Borohydrides

The alanates have numerous isostructural counterparts in the borohydrides¹⁷ (e.g., NaBH₄). The borohydrides tend to be more thermodynamically stable than the alanates, yet less water-reactive. Can the borohydrides be made to respond to catalysis in a manner similar to the alanates? If so, will new problems arise, such as the production of toxic gaseous boranes?

Transition-Metal Complexes

There are a large number of transitionmetal complex hydrides that have TMH_x complexes analogous to the $[AlH_4]^{1-}$ alanate

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complexes, for example, the [FeH₆]⁴⁻ complex in Mg₂FeH₆.²¹ There are numerous such complex hydrides that have been discovered by groups led by Yvon in Geneva,²¹ Bronger in Aachen,²² and Noréus in Stockholm,23 among others. In most cases, they are reversible only with difficulty, although at least in the case of Mg₂FeH₆, excellent cyclic capacity can be seen, even in the uncatalyzed state.24 Although some of these hydrides are too stable for low-temperature use, demonstrations of improved (catalyzed) reversibility in the transition-metal complex hydrides would open a new hydride world of opportunities.

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Supplementary Information

For more information on international cooperative efforts toward solving the H₂ storage problem with metal hydrides and carbon, see URL http://hydpark.ca.

sandia.gov/iea.html to view the activities in Task 17 of the International Energy Agency Hydrogen Implementing Agreement.

References

- 1. B. Bogdanović and M.J. Schwickardi, J. Alloys Compd. 253 (1997) p. 1.
- 2. B. Bogdanović, R.A. Brand, A. Marjanović, M. Schwickardi, and J. Tölle, J. Alloys Compd. 302 (2000) p. 36.
- 3. Millennium Cell Inc. Home Page, http:// www.millenniumcell.com (accessed July 2002); H-GeneTech Alliance, http://alliance. hydrogen.co.jp (accessed July 2002).
- 4. T.N. Dymova, N.G. Eliseeva, S.I. Bakum, and Yu.M. Dergachev, Dokl. Akad. Nauk SSSR 215 (1974) p. 1369, Engl. p. 256.
- 5. T.N. Dymova, Yu.M. Dergachev, V.A. Sokolov, and N.A. Grechanaya, Dokl. Akad. Nauk SSSR 224 (1975) p. 591, Engl. p. 556.
- 6. C.M. Jensen, R.A. Zidan, N. Mariels, A.G. Hee, and C. Hagen, Int. J. Hydrogen Energy 24 (1999) p. 461.
- 7. R.A. Zidan, S. Takara, A.G. Hee, and C.M. Jensen, J. Alloys Compd. 285 (1999) p. 119.
- 8. A. Zaluska, L. Zaluski, and J.O. Ström-Olsen, J. Alloys Compd. 298 (2000) p. 125.
- 9. G. Sandrock, K. Gross, G. Thomas, C. Jensen, D. Meeker, and S. Takara, J. Alloys Compd. 330-332 (2002) p. 696.
- 10. C.M. Jensen and K.J. Gross, Appl. Phys. A 72 (2001) p. 213.
- 11. K.J. Gross, G.J. Thomas, and C.M. Jensen,

I. Alloys Compd. 330-332 (2002) p. 683.

- 12. G. Sandrock, K. Gross, and G. Thomas, J. Alloys Compd. 339 (2002) p. 299.
- 13. K.J. Gross, G. Sandrock, and G. Thomas, J. Alloys Compd. 330-332 (2002) p. 691.
- 14. G.J. Thomas, K.J. Gross, and N. Yang, J. Alloys Compd. 330-332 (2002) p. 702.
- 15. D. Sun, T. Kiyobayashi, H.T. Takeshita, N. Kuriyama, and C.M. Jensen, J. Alloys Compd. 337 (2002) p. L8.
- 16. V.P. Balema, K.W. Dennis, and V.K. Pecharsky, Chem. Commun. (2000) p. 1665.
- 17. E.A. Sullivan, in Kirk-Othmer Encyclopedia of Chemical Technology, Vol. 13 (John Wiley & Sons, New York, 1995) p. 606.
- 18. B. Bogdanović and M.J. Schwickardi, Appl. Phys. A 72 (2001) p. 221.
- 19. A. Zaluska, L. Zaluski, and J.O. Ström-Olsen, Appl. Phys. A 72 (2001) p. 157.
- 20. K.J. Gross, G.J. Thomas, E. Majzoub, and G. Sandrock, in Proc. 2001 DOE Hydrogen Program Review, NREL/CP-570-30535 (National Renewable Energy Laboratory, Golden, CO, 2001), available from http://www.eren.doe.gov/ hydrogen/docs/30535toc.html (accessed July
- 21. K. Yvon, Chimia 52 (1998) p. 613.
- 22. W. Bronger, J. Alloys Compd. 225 (1995) p. 1. 23. M. Olofsson-Mårtensson, U. Häussermann, J. Tomkinson, and D. Noréus, J. Am. Chem. Soc. 122 (2000) p. 6960.
- 24. A. Reiser, B. Bogdanović, and K. Schlichte, Int. J. Hydrogen Energy 25 (2000) p. 425.

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